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(54) Title: CHROMIUM SUPPORT-AGGLOMERATE-TRANSITION METAL POLYMERIZATION CATALYSTS AND PROCESSES UTILIZING SAME

(57) Abstract: The present invention is directed to a novel one-step method for forming a supported catalyst complex of high activity by substantially simultaneously contacting a bidentate or tridentate ligand forming compound, a transition metal compound and a chromium immobilized Lewis acid support-agglomerate. The catalyst can be formed prior to polymerization of olefins or within the polymerization reaction zone.

**CHROMIUM SUPPORT-AGGLOMERATE- TRANSITION METAL
POLYMERIZATION CATALYSTS AND PROCESSES UTILIZING SAME**

[0001] The present application is made with respect to co-pending U.S. provisional application Serial No. 60/287,617, filed on April 30, 2001.

FIELD OF THE INVENTION

[0002] The present invention relates to a novel heterogeneous transition metal catalysts that are useful in olefin polymerization and to processes utilizing the same. More specifically, the present invention provides a single step method of forming a supported catalytic complex by substantially simultaneously contacting a bidentate or tridentate ligand forming compound, a transition metal compound and certain chromium immobilized support-agglomerates and recovering the resultant supported catalytic composition or directly utilizing the complex for the catalytic polymerization of olefins. The resultant product exhibits high catalytic activity while not requiring the presence of a separate activator (or cocatalyst) to achieve polymerization of olefins therewith.

BACKGROUND OF THE INVENTION

[0003] The present invention is directed to a single step process of forming a coordination catalyst composition by contacting a bidentate or a tridentate ligand forming compound, a transition metal compound and a chromium immobilized support-agglomerate. Further, the present process provides a coordination catalyst composite which does not require the initial formation and isolation of a bidentate or tridentate transition metal chelate nor the need to treat said chelate with a conventional cocatalyst compound to provide an active catalyst composition. The absence of such cocatalysts eliminates the need to handle flammable or hazardous compounds.

[0004] Coordination catalyst systems, which are usually based on transition metal compounds of Group 3 to 10 and organometallic compounds of Group 13 of the Periodic Table of the Elements, are an exceptionally diverse group of catalysts which

are employed in chemical reactions of olefinically unsaturated compounds for the preparation of olefin polymers by coordination polymerization.

[0005] The preparation of polyethylene of increased density (high-density polyethylene, HDPE) and of polymers and copolymers of ethylene, propylene or other 1-alkenes is of considerable industrial importance. The use of organometallic catalyst for preparation of such polymers and copolymers has become of increasing interest.

[0006] The prevailing belief on the reaction mechanism of coordination catalysts is that the transition metal of the catalyst compound forms a catalytically active center to which the olefinically unsaturated compound bonds by coordination in a first step. Olefin polymerization takes place via coordination of the monomers and a subsequent insertion reaction into a transition metal-carbon or a transition metal-hydrogen bond.

[0007] The presence of activator compounds (e.g., borane, borate or alumoxane compounds such as methylalumoxane) in the coordination catalyst systems or during the catalyzed reaction is thought to be necessary in order to activate the catalyst. The chelate compound containing the transition metal atom is typically referred to as a "pre-catalyst". It is generally believed that certain compounds (e.g. MAO) that are known to be capable of causing alkylation of the transition metal atom and subsequent abstraction of hydrocarbyl group to provide an active catalytic site with respect to the pre-catalyst are required to activate the pre-catalyst. Such compounds are typically referred to as "co-catalysts" and are selected from alkyl alumoxanes or certain borane or borate compounds. The combination of a pre-catalyst with a co-catalyst is generally referred to as a "primary catalyst". These co-catalysts have certain drawbacks that have inhibited the use of the resultant complex in commercial applications. The alumoxanes are pyrophoric and require special handling when used. The borane and borate co-catalysts, although easier to handle, are more expensive due to their formation from reagents that are difficult to handle. Because each of the co-catalysts is used in large amounts to form a resultant catalytic complex system, the concerns related to each are substantial.

[0008] The best-known industrially used catalyst systems for coordination polymerization are those of the "Ziegler-Natta catalyst" type and the "Phillips

catalyst" type. The former comprise the reaction product of a metal alkyl or hydride of an element of the first three main groups of the Periodic Table and a reducible compound of a transition metal element of Groups 4 to 7. The combination used most frequently comprises an aluminum alkyl, such as diethylaluminum chloride and titanium (IV) chloride. For example, it is known that highly active Ziegler-Natta catalysts are systems in which the titanium compound is fixed chemically to the surface of magnesium compounds, such as, in particular, magnesium chloride.

[0009] The Phillips Process for ethylene polymerization developed around Phillips catalyst that is composed of chromium oxide on silica as the support. This catalyst was developed by Hogan and Banks and described in U. S. Patent 2,825,721, as well as A. Clark et al. in Ind. Eng. Chem. 48, 1152 (1956). Commercialization of this process provided the first linear polyalkenes and accounts for a large amount of the high-density polyethylene (HDPE) produced today.

[0010] More recent developments have focused on single-site catalyst systems. Such systems are characterized by the fact that their metal centers behave alike during polymerization to make very uniform polymers. Catalysts are judged to behave in a single-site manner when the polymer they make meets some basic criteria (e.g., narrow molecular weight distribution, or uniform comonomer distribution). Thus, the metal can have any ligand set around it and be classified as "single-site" as long as the polymer that it produces has certain properties. Includable within single-site catalyst systems are metallocene catalysts, and constrained geometry catalysts.

[0011] A "metallocene" is conventionally understood to mean a metal (e.g., Zr, Ti, Hf, Sc, Y, Vi or La) complex that is bound to two cyclopentadienyl (Cp) rings, or derivatives thereof, such as indenyl, tetrahydroindenyl, fluorenyl and mixtures. In addition to the two Cp ligands, other groups can be attached to the metal center, most commonly halides and alkyls. The Cp rings can be linked together (so-called "bridged metallocene" structure), as in most polypropylene catalysts, or they can be independent and freely rotating, as in most (but not all) metallocene-based polyethylene catalysts. The defining feature is the presence of two Cp ligands or derivatives thereof.

[0012] Metallocene catalysts can be employed either as so-called "neutral metallocenes" in which case an alumoxane, such as methylalumoxane, is used as an or they can be employed as so-called "cationic metallocenes" which incorporate a stable and loosely bound non-coordinating anion as a counter ion to a cationic metal metallocene center. Cationic metallocenes are disclosed in U.S. Patent Nos. 5,064,802; 5,225,500; 5,243,002; 5,321,106; 5,427,991; and 5,643,847; and EP 426,637 and EP 426,638.

[0013] "Constrained geometry" is a term that refers to a particular class of organometallic complexes in which the metal center is bound by only one modified Cp ring or derivative. The Cp ring is modified by bridging to a heteroatom such as nitrogen, phosphorus, oxygen, or sulfur, and this heteroatom also binds to the metal site. The bridged structure forms a fairly rigid system, thus the term "constrained geometry". By virtue of its open structure, the constrained geometry catalyst can produce resins (long chain branching) that are not possible with normal metallocene catalysts.

[0014] The above-described single site catalyst systems are primarily based on early transition metal d⁰ complexes useful in coordination polymerization processes. However, these catalysts are known to be oxophilic and, therefore, have low tolerance with respect to even small amounts of oxygenated impurities, such as oxygen, water and oxygenated hydrocarbons. Thus these materials are difficult to handle and use.

[0015] More recently, late transitional metal (e.g., Fe, Co, Ni, or Pd) bidentate and tridentate catalyst systems have been developed. Representative disclosures of such late transition metal catalysts are found in U.S. Patent No. 5,880,241 and its divisional counterparts U.S. Patent Nos. 5,880,323; 5,866,663; 5,886,224; 5,891,963; 6,184,171; 6,174,976; 6,133,138, and PCT International Application Nos. PCT/US98/00316; PCT/US97/23556; PCT/GB99/00714; PCT/GB99/00715; and PCT/GB99/00716.

[0016] It is commonly believed that both single site and late transition metal pre-catalysts typically require activation to form a cationic metal center by an organometal Lewis acid (e.g., methyl alumoxane (MAO)) (characterized as operating through a hydrocarbyl abstraction mechanism). Such activators or cocatalysts are

inclusion of the aforementioned non-silica gel constituents permitted to be present in Component A of the support-agglomerate.

[0087] Component B forming the support-agglomerate is a layered material having a three-dimensional structure, which exhibits the strongest chemical bonds in only two dimensions. More specifically, the strongest chemical bonds are formed in and within two dimensional planes which are stacked on top of each other to form a three dimensional solid. The two dimensional planes are held together by weaker chemical bonds than those holding an individual plane together and generally arise from Van der Waals forces, electrostatic interactions, and hydrogen bonding. The electrostatic interactions are mediated by ions located between the layers and in addition, hydrogen bonding can occur between complimentary layers or can be mediated by interlaminar bridging molecules.

[0088] Representative examples of suitable layered materials includable in layered Component B can be amorphous or crystalline, preferably amorphous. Suitable layered Component B materials include clay, and clay minerals.

[0089] Clay is typically composed of clay minerals (i.e., crystalline silicate salts) as the main constituent. The clay or clay mineral is usually an inorganic polymeric compound of high molecular complexity constituted by a tetrahedral unit in which a central silicon atom coordinates oxygen atoms and an octahedral unit in which a central aluminum, magnesium or iron atom coordinates oxygen or hydroxide. The skeletal structures of many clays or clay minerals are not electrically neutral and have positive, or more typically, negative charges on their surfaces. When possessing a negatively charged surface, they have cations in their interlaminar structures to complement such negative charges. Such interlaminar cations can be ion-exchanged by other cations. A quantification of a clay's ability to exchange interlaminar cations is called its cation exchange capacity (CEC) and is represented by milliequivalents (meq) per 100 g of clay. CEC differs depending upon the type of clay, and Clay Handbook, second edition (compiled by Japanese Clay Association, published by Gihodo Shuppan K.K.) gives the following information: Kaolinite; 3 to 15 meq/100 g, halloysite; 5 to 40 meq/100 g, montmorillonite; 80 to 150 meq/100 g, illite; 10 to

40 meq/100 g, vermiculite; 100 to 150 meq/100 g, chlorite; 10 to 40 meq/100 g, zeolite•attapulgite; 20 to 30 meq/100 g. Thus, layered Component B to be used in the present invention, is a material, e.g., clay or clay mineral, typically having its surface negatively charged and preferably also having the ability to exchange cations.

[0090] Thus, clay minerals generally have the characteristic layer structure described above, containing between the layers, various levels of negative charges. In this respect, the clay mineral is substantially different from metal oxides having a three-dimensional structure such as silica, alumina, and zeolite. The clay minerals are classified according to the levels of the aforementioned negative charge for the chemical formula: (1) biophilite, kaolinite, dickalite, and talc having the negative charge of 0 (zero), (2) smectite having the negative charge of from -0.25 to -0.6, (3) vermiculite having the negative charge of from -0.6 to -0.9, (4) mica having the negative charge of from about -1, and (5) brittle mica having a negative charge of about -2. Each of the above groups includes various minerals. For example, the smectite group includes montmorillonite, beidellite, saponite, nontronite, hectorite, teniolite, suconite and related analogues; the mica group includes white mica, palagonite and illite. These clay minerals exist in nature, and also can be synthesized artificially with a higher purity.

[0091] Any of the natural and artificial clay minerals having a negative charge below 0 are useful in the present invention. The presently preferred clay is montmorillonite, e.g., sodium montmorillonite.

[0092] Further, clays and clay minerals may be used as they are without subjecting them to any treatment prior to formation of the support therefrom, or they may be treated by ball milling, sieving, acid treatment or the like prior to such formation. Further, they may be treated to have water added and adsorbed or may be treated for dehydration under heating before support formation. They may be used alone or in combination as a mixture of two or more of them for support-activation synthesis.

[0093] Component B preferably has a pore volume of pores having a diameter of at least 40 Å (e.g., 40-1000 Å) as measured by a mercury intrusion method employing a mercury porosimeter of at least 0.1 cc/g, more preferably from 0.1 to 1 cc/g. The

average particle size of Component B can vary typically from about 0.01 to about 50, preferably from about 0.1 to about 25, and most preferably from about 0.5 to about 10 microns.

[0094] Although such treatments are not preferred or required to obtain the benefits of the present invention and, therefore, may be excluded, the clays suitable for use as Component B of the support-agglomerate may be subjected to pretreatment with chemicals prior or subsequent to support formation. Examples of the chemical pretreatment include treatment with an acid or alkali, treatment with a salt, and treatment with an organic or inorganic compound. The last treatment can result in formation of a composite material.

[0095] The treatment of the clay minerals with the acid or alkali may not only remove impurities from the mineral, but also may elute part of metallic cations from the crystalline structure of the clay, or may destructively alter the crystalline structure into an amorphous structure.

[0096] Examples of the acids used for this purpose are Brønstead acids, such as hydrochloric, sulfuric, nitric, acetic acid and the like. Sodium hydroxide, potassium hydroxide and calcium hydroxide are preferably used as alkali chemical in the alkali pretreatment of the clay mineral.

[0097] In the case where the clay mineral is pretreated with a salt or an inorganic, or organic compound to give a composite material, the crystalline structure may be retained substantially without being broken and, rather a product that has been modified by ion-exchange may be obtained. Examples of the inorganic salt compounds that may be used in the pretreatment with salts include ionic halide salts, such as sodium chloride, potassium chloride, lithium chloride, magnesium chloride, aluminum chloride, iron chloride and ammonium chloride; sulfate salts, such as sodium sulfate, potassium sulfate, aluminum sulfate and ammonium sulfate; carbonate salts, such as potassium carbonate, sodium carbonate and calcium carbonate; and phosphate salts, such as sodium phosphate, potassium phosphate, aluminum phosphate and ammonium phosphate. Examples of the organic salt

compounds include sodium acetate, potassium acetate, potassium oxalate, sodium citrate, sodium tartarate and the like.

[0098] As examples of the inorganic compound used for the synthesis of inorganic composite material, metal hydroxides that yield hydroxide anions, for example, aluminum hydroxide, zirconium hydroxide, chromium hydroxide and the like may be mentioned.

[0099] In the case where the clay mineral is treated with an organic compound, such compounds will typically comprise a Lewis basic functional group containing an element of the Group 15 or 16 of the Periodic Table, such as organoammonium cation, oxonium cation, sulfonium cation, and phosphonium cation. The organic compound may also preferably comprise a functional group other than the Lewis basic functional group, such as carbonium cation, tropylium cation, and a metal cation. After undergoing such treatment, the exchangeable metallic cations originally present in the clay mineral are exchanged with the enumerated organic cations. Thus, compounds that yield a carbon cation, for example, trityl chloride, tropylium bromide and the like; or a complex compound that yields metallic complex cation, for example a ferrocenium salt and the like; may be used as the organic compound in the pretreatment. In addition to these compounds, onium salts may be used for the same purpose.

[00100] Particular examples of guest organic cations that may be introduced for modification of the clay minerals, include: triphenylsulfonium, trimethylsulfonium, tetraphenylphosphonium, alkyl tri(o-tolyl) phosphonium, triphenylcarbonium, cycloheptatrienium, and ferrocenium; ammonium ions, for example aliphatic ammonium cations, such as butyl ammonium, hexyl ammonium, decyl ammonium, dodecyl ammonium, diethyl ammonium, tributyl ammonium, and N, N-dimethyl decyl ammonium; and aromatic ammonium cations such as anilinium, N-methyl anilinium, N,N-dimethyl anilinium, N-ethyl anilinium, N,N-diethyl anilinium, benzyl ammonium, toluidinium, dibenzyl ammonium, tribenzyl ammonium, N,N-2,4,6-pentamethyl anilinium and the like; and also oxonium ions, such as dimethyl oxonium, diethyl oxonium and the like. These examples are not limiting.

[00101] Ion exchange of the exchangeable cations in the clay mineral with selected organic cations is typically brought about by contacting the clay with an onium compound (salt) comprising the organic cations.

[00102] Particular examples of the onium salts which may be used, include: ammonium compounds; for example aliphatic amine hydrochloride salts, such as propylamine HCl salt, isopropylamine HCl salt, butylamine HCl salt, hexylamine HCl salt, decylamine HCl salt, dodecylamine HCl salt, diethylamine HCl salt, tributylamine HCl salt, triethylamine HCl salt, N,N-dimethyl decylamine HCl salt, N,N-dimethyl undecylamine HCl salt and the like; aromatic amine hydrochloride salts, such as aniline HCl salt, N-methylaniline HCl salt, N,N-dimethylaniline HCl salt, N-ethylaniline HCl salt, N,N-diethylaniline HCl salt, o-toluidine HCl salt, p-toluidine HCl salt, N-methyl-o-toluidine HCl salt, N-methyl-p-toluidine HCl salt, N,N-dimethyl-o-toluidine HCl salt, N,N-dimethyl-p-toluidine HCl salt, benzylamine HCl salt, dibenzylamine HCl salt, N,N-2,4,6-pentamethyl aniline HCl salt and the like; hydrofluoric, hydrobromic and hydroiodic acid salts and sulfate salts of the above-listed aliphatic and aromatic amines; and oxonium compounds, such as hydrochloric acid salts of methyl ether, ethyl ether, phenyl ether and the like. Of the onium compounds the exemplified ammonium or oxonium compounds, preferably the ammonium compounds and more preferably the aromatic amine salts are employed in the modification of the clay mineral.

[00103] The onium compound to be reacted with the clay mineral may be in the isolated form. Alternatively, the onium compound may be formed in situ, for example by contacting the corresponding amine compound, a heteroatom-containing compound, such as an ether or sulfide compound, and a proton acid, such as hydrofluoric, hydrochloric, hydroiodic or sulfuric acid, in the reaction solvent in which the clay mineral is to be pretreated subsequently. The reaction conditions under which the clay mineral can be modified by the onium compound are not critical. Also the relative proportions of the reactants used therein are not critical. Preferably, however, when used the onium compound is employed in a proportion of not less than 0.5 equivalents per equivalent of the cation present in the clay mineral, and more

preferably in a proportion of at least equivalent amount. The clay mineral may be used singly or in admixture with other clay mineral or minerals. Also the onium compound may be used singly or in admixture with other onium compounds.

[00104] The reaction solvent used in the modification pretreatment process may be water or a polar organic solvent. Examples of the organic solvents which may be used suitably, include alcohols, such as methyl alcohol, ethyl alcohol and the like; acetone, tetrahydrofuran, N,N-dimethyl formamide, dimethylsulfoxide, methylene chloride and the like. The solvent may be used singly or as a mixture of two or more solvents.

Preferably, water or an alcohol is employed.

[00105] What can be viewed as separate and distinct classes of chemical modification treatments to which the clays can be subjected to is referred to as pillaring and delamination. Pillaring is a phenomena whereby the platelets of certain clays, such as smectite clays, which are swellable, are separated by intercalation of large guest cations between the negatively charged platelet sheets, which cations function as molecular props or pillars separating the platelets and preventing the layers from collapsing under Van der Waals forces.

[00106] Pillared clays are typically prepared by reacting a smectite clay, such as montmorillonite, with polyoxymetal cations such as polyoxycations of aluminum and zirconium. The reaction product is normally dried in air and calcined to convert the intercalated cations into metal oxide clusters interposed between the platelets of the clay such that the spacing between the platelets ranges from about 6 to about 10 Angstroms and is maintained at such values when the clay is heated to a temperature between about 500°C and 700°C. When the reaction product is dried, the clay platelets, which are propped apart by the metal oxide clusters, orient themselves face-to-face, thereby forming a lamellar structure which yields an X-ray diffraction pattern containing distinct first order or (001) reflection. The extent of lamellar ordering is indicated by the X-ray powder diffraction pattern of the pillared clay. A well ordered, air-dried, pillared montmorillonite may exhibit six or more orders of reflection. Pillared clays and their preparation are described more fully in the article entitled "Intercalated Clay Catalysts," *Science*, Vol. 220, No. 4595 pp. 365-371 (April 22,

1983) and in U.S. Pat. Nos. 4,176,090; 4,216,188; 4,238,364; 4,248,739; 4,271,043; 4,367,163; 4,629,712; 4,637,992; 4,761,391; 4,859,648; and 4,995,964. The disclosures of the aforementioned articles and patents are incorporated herein by reference in their entireties.

[00107] In contrast to pillared clays, which have platelets that are ordered in a face-to-face arrangement, delaminated clays also contain large cations but the platelets are oriented edge-to-edge and edge-to-face in what can be described as a "house-of-cards" structure containing macropores of a size typically found in amorphous aluminosilicates in addition to the micropores found in pillared clays. (See U.S. Pat. No. 4,761,391 for a further discussion.) Such clays are distinct from those that have been subjected to exfoliation by high shear forces and the like which substantially destroys the house of cards structure. Thus, non-exfoliated clays should be used and non-delaminated and non-exfoliated clays are preferred.

[00108] While it is possible and permissible to modify Component B with guest cations as described above, such procedures add process steps to the overall preparation, and from a process point of view, are preferably not employed.

[00109] However, when Component (B) is modified by exchanging originally present cations, the goal sought to be achieved by such exchange is to render the support-activator agglomerate capable of activating either the pre-catalyst or the pre-activated catalyst as described above. It is believed that the indigenous cations typically present in the aforementioned clays are already capable of accomplishing this goal.

[00110] The support-agglomerate is made from an intimate admixture of Components A and B, which admixture is shaped in the form of agglomerate. The weight ratio of Component A to Component B in the agglomerate can vary typically from about 0.25:1 to about 99:1, preferably from about 0.5:1 to about 20:1, most preferably from about 1:1 to about 10:1 (e.g., 4:1).

[00111] The term "agglomerate" refers to a product that combines particles which are held together by a variety of physical-chemical forces. More specifically, each agglomerate is preferably composed of a plurality of contiguous, constituent primary

particles derived primarily from Component A and much smaller secondary constituent particles derived from both Component A and Component B preferably joined and connected at their points of contact.

[00112] The agglomerates of the present invention preferably will exhibit a higher macropore content than the constituent primary or secondary particles as a result of the interparticle voids between the constituent particles. However, such interparticle voids may be almost completely filled with the smaller secondary particles in other embodiments of the spray-dried agglomerates.

[00113] The agglomeration of Components (A) and (B) may be carried out in accordance with methods well known to the art, such as by pelletizing, extrusion, shaping into beads in a rotating coating drum, and the like. A nodulizing technique whereby composite particles having a diameter of not greater than about 0.1 mm are agglomerated to particles with a diameter of at least about 1 mm by means of a granulation liquid may also be employed.

[00114] The preferred agglomerates are made by drying, preferably spray drying, a slurry of Components A and B. More specifically, in this embodiment, the support is made by admixing Components A and B to form a slurry, preferably an aqueous slurry, comprising typically at least 50, preferably at least 75 (e.g., at least 80), and most preferably at least 85 (e.g., at least 90), wt. % water based on the slurry weight. However, organic solvents, such as C₅ to C₁₂ alkanes, alcohols (e.g. isopropyl alcohol), may also be employed although they represent a fire hazard relative to water and often make agglomerates too fragile for use as polymerization catalysts.

[00115] To render Component A suitable for agglomerate formation, e.g. drying or spray drying, various milling procedures are typically employed (although not required). The goal of the milling procedure is to ultimately provide Component A, when intended to be spray dried, with an average particle size of typically from about 2 to about 10 (e.g. 3 to about 7) preferably from about 4 to about 9, and most preferably from 4 to 7 microns. Desirably the milling procedures will also impart a particle size Distribution Span to the particles in the slurry of typically from 0.5 to

about 3.0, and preferably from about 0.5 to about 2.0. The particle size Distribution Span is determined in accordance with the following equation.

$$\text{Distribution Span} = \frac{D_{90} - D_{10}}{D_{50}} \quad \text{Equation 1a}$$

wherein D_{10} , D_{50} , and D_{90} represent the 10th, 50th, and 90th percentile, respectively, of the particle size (diameter) distribution, i.e. a D_{90} of 100 microns means that 90 volume % of the particles have diameters less than or equal to 100 microns. Still more preferably, the milling is conducted to impart a particle size distribution to the Component A inorganic oxides in the slurry to be spray dried such that the Component A colloidal content is typically from about 2 to about 60 (e.g. 2 to about 40), preferably from about 3 to about 25, and most preferably from about 4 to about 20 wt.

[00116] The colloidal content of Component A to be spray dried is determined by centrifuging a sample for 30 minutes at 3600RPM. The liquid (supernatant) which remains on top of the test tube is decanted, and analyzed for % solids. The % of colloidal material is then determined by the following equation:

$$\% \text{ colloid} = \left[\frac{\left(\frac{1 - B}{B} \right) - 2.2}{\left(\frac{1 - A}{A} \right) - 2.2} \right] \times 100 \quad \text{Equation 1b}$$

wherein

A = wt. solids in supernatant/100, and

B = wt. solids of original slurry/100

[00117] The colloidal content will possess a particle diameter in the colloidal range of typically less than about 1, preferably less than about 0.5, and typically from about

0.4 to about 1 micron. All particle size and particle size distribution measurements described herein are determined by a Mastersizer® unit from Malvern Instruments, which operates on the principle of laser light diffraction and is known to all familiar in the art of small particle analysis.

[00118] As the dry colloidal content of the Component A slurry exceeds about 60 wt. %, the constituent particles of the agglomerate can become bound too tightly together. Conversely, while the presence of at least some colloidal content of the slurry is desired, a slurry containing no colloidal content (e.g. dry milled powder alone) can produce agglomerates of the support which have extremely low physical integrity to an undesirable degree. In such instances, it may be desirable to include some alternative source of binder. Thus, it is preferred that the colloidal content of the Component A (as dry solids) be within the range of from about 5 to 50, more preferably from 5-40 wt.%.

[00119] One milling procedure, which has been found to impart the above-described properties as well as the desired morphology, involves a wet milling procedure and optionally a dry milling procedure. A wet milling procedure is characterized by the presence of liquid, e.g. water, during the milling procedure. Thus, wet milling is typically performed on a slurry of the inorganic oxide particles having a solids content of typically from about 15 to about 25 weight % based on the slurry weight.

[00120] In the wet milling procedure, the washed inorganic oxide is typically subjected to a milling procedure well known in the art that is necessary to produce slurries with the particle sizes specified above. Suitable mills include hammer mills, impact mills (where particle size reduction/control is achieved by impact of the oxide with metal blades and retained by an appropriately sized screen), and sand mills (where particle size control/reduction is achieved by contact of the oxide with hard media such as sand or zirconia beads).

[00121] The colloidal particles within the wet milled material are the primary source of the colloid content in the slurry to be spray dried as described above, and are believed to act as a binder upon spray drying.

[00122] More specifically, with wet milling, Component A can be slurried in a media (usually water) and the mixture then subjected to intense mechanical action, such as the high speed blades of a hammer mill or rapidly churning media of a sand mill. Wet milling reduces particle size and produces colloidal silica as well.

[00123] Accordingly, the inorganic oxide (typically while still wet) is then subjected to a milling operation as described below to prepare it for spray drying. Once the target average particle size and preferably the particle size Distribution Span is imparted to Component A, a slurry, preferably aqueous slurry, is prepared for agglomeration, preferably by spray drying.

[00124] A dry milling procedure is characterized by the substantial absence of the presence of free flowing liquid, e.g. water or solvent. Thus, while the final dry milled material may contain some absorbed moisture, it is essentially in powder form, not a suspension or solution of particles in liquid. The dry milling refers typically to a process that takes particulate inorganic oxide and reduces it in size by some mechanical action impingement onto a metal surface, or collision with other particles after entrainment into a high-velocity air stream or the like.

[00125] The dry milling referred to typically takes particulate inorganic oxide and reduces it in size either by mechanical action, impingement onto a metal surface, or collision with other particles after entrainment into a high-velocity air stream.

[00126] In the dry milling procedure, Component (A) is typically milled in a manner sufficient to reduce its average particle size to typically from about 2 to about 10, preferably from about 3 to about 7, and most preferably from about 3 to 6 microns, and its moisture content to typically less than about 50, preferably less than about 25, and most preferably less than about 15 weight %. In order to attain the dry milling particle size targets at the higher moisture contents, it may be necessary to conduct dry milling while the particles are frozen.

[00127] The dry milling is also conducted to preferably impart a particle size distribution such that the Distribution Span is typically from about 0.5 to about 3.0, preferably from about 0.5 to about 2.0, and most preferably from about 0.7 to about

1.3. Thus, the resulting dry milled material exists in the form of a powder prior to being slurried for spray drying.

[00128] The dry milling is preferably conducted in a mill capable of flash drying the inorganic oxide while milling. Flash drying is a standard industrial process where the material to be dried is quickly dispersed into a hot air chamber and exposed to an air stream of 370 - 537°C. The rate of air and material input is balanced such that the temperature of the outgoing air and the material entrained in it is generally 121 - 176°C. The whole process of drying usually takes place in less than 10 seconds, reducing the moisture content to less than about 10%. Alternatively, the inorganic oxide can be separately flash dried to the aforescribed moisture content in a flash dryer and then placed in a dry mill and milled. Suitable dry mills include an ABB Raymond™ impact mill or an ALJET™ FLUID ENERGY MILL. Ball mills can also be used. Suitable flash drying equipment includes Bowen™ flash dryer. Other similar equipment is well known in the chemical processing industry.

[00129] Flash drying is typically accomplished by exposing the inorganic oxide to conditions of temperature and pressure sufficient to reduce the moisture content thereof to levels as described above over a period of time of typically less than about 60, preferably less than about 30, and most preferably less than about 5 seconds. Dry milling typically does not produce colloidal silica.

[00130] In accordance with one embodiment of the agglomerate formation by spray drying, at least a portion of the material constituting Component A is derived from wet milling, and optionally but preferably at least a portion is derived from dry milling. Thus, prior to agglomeration, Component A will typically comprise a mixture of previously wet milled inorganic oxide, e.g. silica gel, and dry milled inorganic oxide, e.g. silica gel powder. More specifically, the weight ratio (on a dry solids content basis as defined hereinafter) of the wet milled/dry milled inorganic oxide solids in the slurry can vary typically from about 9:0 to about 0.1:1 (e.g., 9:1), preferably from about 1.5:1 to about 0.1:1, and most preferably from about 0.6:1 to about 0.25:1. The particular wet milled/dry milled solids ratio of Component A

employed will be selected to achieve the target properties in the final slurry to be used in agglomerate formation.

[00131] In an alternative embodiment, a sequential milling procedure can be employed to impart the target properties of average particle size and particle size distribution. The sequential milling procedure involves dry milling a sample of the Component A inorganic oxide and then wet milling the previously dry milled sample.

[00132] It has been observed that drying of inorganic oxide starting material during dry milling and then using the dry milled product for wet milling tends to produce a lower colloidal content relative to mixing a separately prepared dry milled product and a separately prepared wet milled product. The reason for this phenomenon is not entirely understood. However, sufficient colloidal content is produced to bind the agglomerate together in a desirable manner.

[00133] Once the target average particle size and preferably the particle size distribution span is imparted to Component (A), a slurry, preferably an aqueous slurry, is prepared for agglomeration, preferably by spray drying.

[00134] The Component (B) layered material, e.g. clay, is typically comprised of fine particles having an average particle size of typically less than 10, preferably less than 5, and most preferably less than 1 micron, such particle sizes ranging typically from about 0.1 to about 10, preferably from about 0.1 to about 5, and most preferably from about 0.1 to about 1 microns. Other preferable physical properties of the clay include a total nitrogen pore volume of typically greater than 0.005 (e.g., 0.005 to 1.50), preferably greater than about 0.1 (e.g., 0.1 to 2) cc/g; a nitrogen surface area of typically greater than 10, preferably greater than 30 (e.g., 10 to 100) m²/g; and an Apparent Bulk Density (ABD) of typically greater than 0.10, preferably greater than 0.25 (e.g., 0.10 to 0.75) g/cc. Milling procedures can be employed to achieve these target properties, if necessary.

[00135] To agglomerate by spray drying, Components (A) and (B) are admixed, typically in a suitable diluent, to form a slurry of the same. The diluent can be aqueous or organic. The preferred liquid slurry medium for spray drying is aqueous,

typically greater than 75, preferably greater than 80, and most preferably greater than 95 wt. % water (e.g. entirely water).

[00136] The weight ratio of Component (A) to Component (B) in the slurry, can vary typically from about 0.25:1 to about 99:1, preferably from about 0.5:1 to about 20:1, and most preferably from about 1:1 to about 10:1 (e.g., 4:1). The solids content of the slurry containing the mixture of Components-A and -B can vary typically from about 5 to about 25, preferably from about 10 to about 20, and most preferably from about 15 to about 20 wt.% based on the slurry weight.

[00137] Accordingly, agglomerate formation is controlled to impart preferably the following properties to the support-agglomerate:

- (1) A surface area of typically at least about 20, preferably at least about 30, and most preferably from at least about 50 m²/g, which surface area can range typically from about 20 to about 800, preferably from about 30 to about 700, and most preferably from about 50 to about 600 m²/g;
- (2) A bulk density of the support-agglomerate particles of typically at least about 0.15, preferably at least about 0.20, and most preferably at least about 0.25 g/ml, which bulk density can range typically from about 0.15 to about 1, preferably from about 0.20 to about 0.75, and most preferably from about 0.25 to about 0.45 g/ml;
- (3) An average pore diameter of typically from about 30 to about 300, and most preferably from about 60 to about 150 Angstroms;
- (4) A total pore volume of typically from about 0.10 to about 2.0, preferably from about 0.5 to about 1.8, and most preferably from about 0.8 to about 1.6 cc/g; and
- (5) An attrition resistance which provides friability for suitable catalyst fragmentation for the particular polymerization process contemplated.

[00138] The particle size and particle size distribution sought to be imparted to the support-agglomerate particles is dictated and controlled by the type of polymerization reaction in which the ultimate supported catalyst will be employed. For example, a solution polymerization process typically can employ an average particle size of from

about 1 to about 10 microns; a continuous stirred tank reactor (CSTR) slurry polymerization process of from about 8 to 50 microns; a loop slurry polymerization process of from about 10 to about 150 microns; and a gas phase polymerization process of from about 20 to about 120 microns. Moreover, each polymer manufacturer has its own preferences based on the particular reactor configuration.

[00139] Once the desired average particle size is determined for the support-agglomerate based on the targeted polymerization process, the particle size distribution will desirably be such that the Distribution Span is typically from about 0.5 to about 4, preferably from about 0.5 to about 3, and most preferably from about 0.5 to 2.

[00140] Accordingly, as a generalization, the average particle size of the support-agglomerate will range typically from about 4 to about 250 (e.g. about 8 to about 200), and preferably from about 8 to about 100 (e.g. about 30 to about 60) microns.

[00141] When the support-agglomerate is formed by spray drying, they can be further characterized in that typically at least 80, preferably at least 90, and most preferably at least 95 volume % of that fraction of the support-agglomerate particles smaller than the D₉₀ of the entire agglomerate particle size distribution possesses microspheroidal shape (i.e., morphology). Evaluation of the microspheroidal morphology is performed on that fraction of the particle size distribution of the support-agglomerates which are smaller than the D₉₀ to avoid distortion of the results by a few large particle chunks which because of their large volume, would constitute a non-representative sample of the agglomerate volume. The term "spheroidal" as used herein means small particles of a generally rounded, but not necessarily spherical shape. This term is intended to distinguish from irregular jagged chunks and leaf or rod like configurations. "Spheroidal" is also intended to include polylobed configurations wherein the lobes are also generally rounded, although polylobed structures are uncommon when the agglomerate is made as described herein.

[00142] Each microspheroid is preferably composed of a loosely to densely packed composite of Components (A) and (B) typically with some, to substantially no, interstitial void spaces, and typically substantially no visible boundaries, in an

electron micrograph, between particles originally derived from Components (A) and (B).

[00143] However, microprobe image and elemental analysis of a cross-sectioned view of preferred agglomerate particles reveals that the Fe and Al ions associated with Component-B are distributed in clusters of varying density around discrete sub-particles of material-bearing no iron or aluminum. This leads to the conclusion that, in the most preferred agglomerate particles, Component-B is intimately admixed with Component-A such that islands of inorganic oxide (e.g., silica) are surrounded by a matrix of inorganic oxide (most likely derived from the colloidal constituents of the inorganic oxide) and layered material (e.g., clay). It is believed that the varying intensity (concentration) of Al and Fe, in the matrix is indicative of varying ratios of Component (A) to Component (B) in the matrix.

[00144] The microspheroidal shape of the support significantly enhances the desired morphology of the polymers derived therefrom. Thus, one is able to simultaneously significantly enhance catalyst activity and desired polymer morphology by utilizing chromium immobilized on the 2 components of support-agglomerate.

[00145] The terms "surface area" and "pore volume" refer herein to the specific surface area and pore volume determined by nitrogen adsorption using the B.E.T. technique as described by S. Brunauer, P. Emmett, and E. Teller in Journal of American Chemical society, 60, pp. 209-319 (1939).

[00146] Bulk density is measured by quickly transferring (in 10 seconds) the sample powder into a graduated cylinder, which overflows when exactly 100cc is reached. No further powder is added at this point. The rate of powder addition prevents settling within the cylinder. The weight of the powder is divided by 100cc to give the density.

[00147] Spray drying conditions are typically controlled in order to impart the desired target properties described above to the agglomerate. The most influential spray drying conditions are the pH of the aqueous slurry to be spray dried, as well as its dry solids content. By "dry solids content" as used herein is meant the weight of solids in the slurry after such solids have been dried at 175°C for 3 hours, and then at

955°C for 1 hour. Thus, dry solids content is used to quantify the weight of solid ingredients which exist in the slurry and to avoid inclusion of adsorbed water in such weight.

[00148] Typically, the pH of the slurry will be controlled or adjusted to be from about 5 to about 10 (e.g., 8 to 9), preferably from about 7 to about 9, and the dry solids content will be controlled or adjusted to be typically from about 12 to 30, preferably from about 15 to about 25, and most preferably from about 18 to about 22 (e.g. 20) weight % based on the weight of the slurry and the dry weight of the gel.

[00149] Control of the remaining variables in the spray drying process, such as the viscosity and temperature of the feed, surface tension of the feed, feed rate, the selection and operation of the atomizer (preferably an air atomizer is employed and preferably without the use of a pressure nozzle), the atomization energy applied, the manner in which air and spray are contacted, and the rate of drying, are well within the skill of the spray dry artisan once directed by the target properties sought to be imparted to the product produced by the spray drying. (See for example U.S. Pat. No. 4,131,452.)

[00150] Product separation from the drying air follows completion of the spray drying stage when the dried product remains suspended in the air. Any convenient collection method can be employed, such as removal from the base of the spray dryer by the use of separation equipment.

[00151] The support-agglomerate described above is contacted with a chromium compound, such as a salt, that is at least partially soluble in water (preferred) or an organic liquid. The chromium salt may be contacted with the support-agglomerate either during formation of Component (A) or Component (B) or upon mixing of Components (A) and (B) prior to milling of the combined components and/or prior to agglomeration, such as by spray drying of the components. It is preferred that a solution or suspension of the chromium salt be contacted with a slurry of Components (A) and (B) prior to the agglomeration of the components forming the support-agglomerate, as described herein above.

[00152] The chromium compound suitable for use in forming Component III of the subject catalyst composition of the present invention is preferably selected from any chromium salt of an inorganic or organic acid that has some degree of solubility with respect to the media used to mix the compound with either one of the Components A or B or the resultant support-agglomerate, as applicable. The preferred media is water. For example, suitable inorganic salts are chromium halides, such as chromium dichloride, chromium chloride hexahydrate, chromium dibromide, chromium bromide hexahydrate, chromium tribromide chromium difluoride; as well as chromium nitrate; chromic anhydride, chromium phosphate; chromium^(II) sulfate; chromium sulfate pentadecalhydrate and octadecal hydrate; chromium orthophosphate; and the like and mixtures thereof.

[00153] Organic chromium compounds suitable as a chromium atom source for forming Component III of the present catalyst are water-soluble compounds, such as, for example, salts of organic acids, such as chromium acetate, chromium acetate hydrate, chromium acetylacetone, chromium propionate, chromium oxalate hydrate, chromium oxalate hexahydrate; amine complexes such as hexamine chromium III chloride; chloropentamine chromium chloride; hexaurea chromium III fluorosilicate; chromocene and the like and mixtures thereof.

[00154] Certain chromium compounds found useful herein have greater solubility in organic solvents. These compounds include, for example, chromocene, bis-(triphenylsilyl) chromate and the like. In such instances, the salt may be contacted with Component A or Component B using an organic liquid solution followed by vacuum evaporation of the organic solvent at temperatures of from ambient to about 40°C followed by spray drying or by impregnating the chromium into a previously formed support-agglomerate.

[00155] The preferred chromium compounds are chromium sulfate, chromium nitrate, chromium acetate and chromium acetylacetone. The most preferred chromium compounds are the acetate and nitrate salts of chromium.

[00156] The chromium precursor salt may be complexed with the Lewis acid support-agglomerate described above by:

- (1) contacting an aqueous solution or suspension of the chromium precursor salt with Component (A), such as prior to milling and/or prior to spraying of Component (A);
- (2) contacting an aqueous solution of a mixture of Component (A) and Component (B) prior to milling of this mixture and/or prior to agglomerating the mixture, such as by spray drying; or
- (3) contacting previously formed agglomerated support-promoter attained from Component (A) and Component (B), as described above, with a solution of the chromium precursor salt. This is sometimes called post-impregnation

[00157] In each instance, the chromium compound is introduced as an aqueous or organic solution (solution preferred) or slurry (that is formed from a salt having partial solubility in water). The materials may be contacted for a period of time of from about 15 to about 150 minutes, with from about 15 to 100 minutes being preferred. In certain instances, the materials are mixed for between 15 and 60 minutes and then allowed to remain in the mixer without agitation for a period of up to about 180 minutes. The materials are normally mixed at a temperature of from ambient to about 40° C

[00158] For example, during the formation of Component A of the Lewis-acid support-agglomerate described above, the chromium compound may be added to the silica slurry prior to its agglomeration. Alternately and preferably, the chromium precursor salt may be admixed with the silica gel particles prior to milling or after milling in slurry form just prior to its spray drying.

[00159] Alternately, the chromium compound may be added as part of the salt of an inorganic or organic compound that forms part of the composite of the clay Component B of the present Lewis acid support-agglomerate.

[00160] Still further and preferably, the aqueous solution of the mixture of Component A with Component B may have a chromium compound added to the mixture prior to milling of the mixture of the resultant aqueous slurry and/or prior to forming an agglomerated product by spray drying the slurry (most preferred).

[00161] Finally, a slurry of Lewis acid support-agglomerate product, which has been already produced into its agglomerated form, may be contacted with an aqueous solution of chromium compound and subsequently dried.

[00162] Product separation from the drying air follows completion of the spray drying stage when the dried product remains suspended in the air. Any convenient collection method can be employed, such as removal from the base of the spray dryer by the use of separation equipment.

[00163] The product of the support-agglomerate that has been treated with chromium compound is subjected to oxidation after agglomeration to oxidize the chromium atom to a higher oxidation state (e.g., +3, +4, +6). Chromium in its +3 and +4 oxidation state are preferred. The oxidation will typically be conducted at sufficient temperature and time to reduce the total volatiles to between about 0.1 and 8 wt.% where the total volatiles are determined by measuring the weight loss upon destructive calcination of the sample at 1000°C. However, oxidation will typically be conducted by heating the chromium precursor treated support-agglomerate to temperatures of typically from about 600° to about 1800° F (316° to 983° C), preferably from about 800° to about 1500° F (430° to 816° C), and most preferably from about 800° to about 1000° F (430° to 537° C) for periods of typically from about 1 to about 600 (e.g., 50 to 600), and preferably from about 50 to about 300 minutes. The atmosphere of oxidation should be air or other oxygen-laden gas.

Oxidation should be conducted in manners that will avoid sintering.

[00164] The resultant support-agglomerate has chromium atoms immobilized thereto. The amount of chromium (as Cr) present should be from about 0.1 to 10 weight percent, preferably from about 0.2 to 5 weight percent, and more preferably, from about 0.3 to 2 weight percent (e.g., from about 0.5 to 1.5 weight percent) of the resultant chromium immobilized support-agglomerate described above. Although not limited to the following presumption, it is believed that the chromium atoms of the precursor material are bonded (such as covalently bonded) to the support-agglomerate through oxygen atoms. For example, residual hydroxyl groups of the inorganic oxide may provide sites which react with chromium precursor and result in an oxygen

bridge between the chromium atom and the support-agglomerate. Another example may be the immobilization of the chromium atom to sites associated with Component (B). Thus, the chromium atom may be immobilized with sites associated with Component (A) or Component (B) or with a combination of sites associated with Component (A) and Component (B).

[00165] After formation, the chromium immobilized support-agglomerate is preferably sized prior to oxidation. This can be conveniently accomplished by screening or air classifying as is well known in the art. The particle size and particle size distribution selected will depend on the catalyst type and polymerization process to be applied, as would be well known in the art. Normally, when the catalyst composition of the present invention is contemplated for use in a slurry polymerization process, the particle size of the support-activator agglomerate is from 1 to 100, preferably from 10 to 60 microns.

[00166] Although it is preferred to provide for the catalyst composition of the present invention by contacting a single ligand compound I or its precursor reagents I-Pre with a transition metal compound II and a support-agglomerate III which contains chromium atoms immobilized thereon and/or therein, one may further introduce a second ligand compound I or another set of precursors reagents or a preformed transition metal bidentate or tridentate ligand complex to the single medium containing the other components forming the present catalyst composition.

[00167] Polymerization of olefin monomers can be accomplished by contacting one or more olefinic monomers in the presence of (1) a bidentate ligand I(A) or tridentate ligand I(B) forming compound, described above; (2) a transition metal compound II, also described above; and (3) a chromium immobilized support-agglomerate described above. These components have been found to provide a polymerization catalyst composition. The components (1), (2) and (3) may be contacted together prior to use in a polymerization reaction zone or may be directly introduced into the polymerization reaction zone. The components may be contacted together in any order. For example, Components (1) and (2) may be contacted together followed by introduction of the chromium immobilized support-agglomerate (3). Alternately,

Components (1) and (3) or Components (2) and (3) may, respectively, be contacted together followed by introduction of the remaining component. Preferably, all three components are contacted substantially simultaneously. For example, the components can be introduced substantially simultaneously in a sequential manner over a period of from about 1 second to 60 minutes, preferably from about 30 seconds to 30 minutes and more preferably, from about 1 minute to 10 minutes after completion of the prior introduced component. Alternately, the components can be added concurrently.

[00168] Without wishing to be bound to any particular theory, it is believed that even without separation of the catalyst system from the inert liquid, the ligand forming compounds of Component I and the transition metal compound of Component II very quickly and uniformly adhere to the surface (outer surface of the pores) of the support-activator agglomerate and/or absorbed (penetrate into the inner structure of the support-activator agglomerate particles) with respect to the structure of the support-activator agglomerate of Component III. It is believed that the molecular size and structure of the ligands and the transition metal compounds used herein permits these components to readily penetrate throughout the porous structure of the support-activator agglomerate. Further, they are caused to be dispersed throughout the support-activator agglomerate due to the support's composition and to form a bidentate or tridentate transition metal ligand containing complex (a pre-catalyst specie) which is bound on and/or within the support-activator agglomerate by ionic bonding with the Lewis-acid species of the Component III. The complex or other catalytic structure formed by Components I and II are also physically intercalated within the layered structure of Component III. Thus, the resultant catalyst complex achieved herein results in effective immobilization of the ligand complex onto the support-activator agglomerate matrix and activation of the pre-catalyst complex as a single-site catalyst complex.

[00169] The polymerization of an olefin as well as the copolymerization of more than one olefin can be accomplished by contacting the desired olefin with the polymerization catalyst composition of (1), (2) and (3) and, when none of the

L groups of the transition metal compound is a hydrocarbyl group, an organometallic reagent. Such reagents are well known and include those represented by the formula:



wherein D represents an element of the Group 1, 2 or 13 of the Periodic Table, a tin atom or a zinc atom; each R independently represents a hydrogen atom, a halogen atom, hydrocarbyl, typically C₁ to C₂₄ hydrocarbyl, including C₁ to C₂₄ alkyl or alkoxy and aryl, aryloxy, arylalkyl, arylalkoxy, alkylaryl or alkylaryloxy group having 6 to 24 carbon atoms such as a hydrogen atom, halogen atom (e.g., chlorine fluorine, bromine, iodine and mixtures thereof), alkyl groups (e.g., methyl, ethyl, propyl, pentyl, hexyl, heptyl, decyl, isopropyl, isobutyl, s-butyl, t-butyl), alkoxy groups (e.g., methyoxy, ethoxy, propoxy, butoxy, isopropoxy), aryl groups (e.g., phenyl, biphenyl, naphthyl), aryloxy groups (e.g., phenoxy), arylalkyl groups (e.g., benzyl, phenylethyl), arylalkoxy groups (benzyloxy), alkylaryl groups (e.g., toyl, xylyl, cumenyl, mesityl), and alkylaryloxy groups (e.g., methylphenoxy) provided that at least one R is a hydrogen atom, an alkyl group having 1 to 24 carbon atoms or an aryl, arylalkyl or alkylaryl group having 6 to 24 carbon atoms; and x is the oxidation number of M. The preferred organometallic compounds are those wherein M is aluminum.

[00170] Representative examples of organometallic compounds include alkyl aluminum compounds, preferably trialkyl aluminum compounds, such as trimethyl aluminum, triethyl aluminum, triisopropyl aluminum, triisobutyl aluminum, tri-n-propylaluminum, triisobutylaluminum, tri-n-butylaluminum, triamylaluminum, and the like; alkyl aluminum alkoxides such as ethyl aluminum diethoxide, diisobutyl aluminum ethoxide, di(tert-butyl) aluminum butoxide, diisopropyl aluminum ethoxide, dimethyl aluminum ethoxide, diethyl aluminum ethoxide, di-n-propyl aluminum ethoxide, di-n-butyl aluminum ethoxide, and the like; aluminum alkoxides such as aluminum ethoxide, aluminum propoxide, aluminum butoxide and the like; alkyl or aryl aluminum halides such as diethyl aluminum chloride, ethyl aluminum

dichloride, diisopropyl aluminum chloride and the like; aluminum aryloxides such as aluminum phenoxide, and the like; and mixed aryl, alkyl or aryloxy, alkyl aluminum compounds and aluminum hydrides such as dimethylaluminum hydride, diethylaluminum hydride, diisopropylaluminum hydride, di-n-propylaluminum hydride, diisobutylaluminum hydride, and di-n-butylaluminum hydride. The most preferred organometallic compounds are the trialkyl aluminum compounds.

[00171] In instances where the organometallic compound is used, it can be directly introduced to the polymerization zone in an inert liquid. When so employed by addition directly to the polymerization zone, the ratio of organometallic compound can be defined as a function of the weight of the support-agglomerate. More specifically, the ratio of millimoles (mmol) of organometallic compound to grams of support-agglomerate employed can vary typically from about 0.001:1 to about 100:1, preferably from about 0.01:1 to about 50:1, and most preferably from about 0.1:1 to about 30:1.

[00172] The organometallic reagent, when present as part of the subject catalyst composition, should be present in from 50 μ mole to 0.1 mole, preferably from 100 μ mole to 0.05 mole per gram of chromium oxide/ support-agglomerate, fully described above.

[00173] Components I and/or I-Pre, II and II can be introduced into the inert liquid in any order or substantially simultaneously. It is preferred that, when the components are introduced sequentially, they are introduced in rapid order; that is, without a substantial period of delay between each components introduction. For example, the components can be introduced sequentially over a period of from about 1 second to 60 minutes, preferably from about 30 seconds to 30 minutes, and more preferably from about 1 minute to 10 minutes after introduction of the prior component. Alternately, the components can be introduced concurrently.

[00174] The mixing of at least one ligand forming compound (I), or alternately, reactants (I-Pre) capable of directly forming a ligand(all referred to in the following discussion as Component (I), transition metal compound (II)(referred to in the following discussion as Component II), and support-agglomerate (III)(referred to in

the following discussion as Component III) can be readily accomplished by introducing the components into a liquid, preferably a substantially inert (with respect to chemical reaction with Components I, II and III) liquid, which can serve as a diluent or solvent for one or more of the catalyst's components.

[00175] Suitable inert liquids include hydrocarbon liquids, preferably C₅-C₁₀ aliphatic or cycloaliphatic hydrocarbons, or C₆-C₁₂ aromatic or alkyl substituted aromatic hydrocarbons and mixtures thereof. The inert liquid may also be selected from certain inert oxyhydrocarbon liquids, such as a C₁-C₈ alkanol, such as methanol, ethanol, isopropanol, butanol and the like; an di(C₁-C₃alkyl)ether, such as diethyl ether, ethyl propyl ether and the like; a cyclic ether, such as tetrahydrofuran, glyme, diglyme and the like; and alkyl aldehydes and ketones. These liquids may be used to form the catalyst composition according to the present invention and removed prior to the composition being introduced into the polymerization zone. Alternately, the liquid used can be chosen from those that may be inert with respect to the polymerization process contemplated (e.g. C₄-C₁₂ alkanes) and, therefore, may be used as the liquid to form the catalyst composition and to introduce the formed composition into the polymerization zone. Still further, when the liquid is inert with respect to the polymerization process (the monomer and the resultant polymer), the composition may be formed in-situ in the polymerization zone by introducing the Components I, II and III directly to the polymerization zone.

[00176] The components are introduced into the liquid and maintained therein under agitation and at low temperature and pressure conditions. Particularly suitable hydrocarbons include, for example, 1,2-dichloroethane, dichloromethane, pentane, isopentane, hexane, heptane, octane, iso-octane, nonane, isononane, decane, cyclohexane, methylcyclohexane, toluene, and combinations of two or more of such diluents. Ethers such as diethyl ether and tetrahydrofuran can also be used.

[00177] Components I and/or I-Pre, II and III can be introduced into the inert liquid in any order or substantially simultaneously. It is preferred that, when the components are introduced sequentially, they are introduced in rapid order; that is, without a substantial period of delay between each component's introduction. For

example, the components can be introduced sequentially over a period of from about 1 second to 60 minutes, preferably from about 30 seconds to 30 minutes, and more preferably from about 1 minute to 10 minutes.

[00178] The temperature of the liquid into which the components are added may range typically from about 0 to about 200°C, preferably from about 5 to about 150°C, and most preferably from about 20 to about 100°C (e.g. 60 to about 100°C). The Components can be contacted at reduced, atmospheric or elevated pressure. Ambient conditions are preferred. The atmospheric condition of the mixing zone should preferably be substantially anaerobic and anhydrous.

[00179] The components are mixed for a period, preferably from 0.5 hour to 24 hours, more preferably from 1 to 12 hours and most preferably from 1 to 5 hours to provide a substantially uniform catalyst composition.

[00180] When the catalyst composition is formed outside of the polymerization zone, the formed product can be separated from the inert liquid, by filtration, vacuum distillation or the like to provide a solid preformed catalyst composition.

[00181] The solid preformed catalyst is preferably stored under anaerobic conditions until being introduced into a polymerization reaction zone for use in forming polyolefin products. The resultant catalyst composition is storage stable for about 3 to 6 months or longer.

[00182] Alternatively, the mixture of Components I, II and III in the inert liquid hydrocarbon (with respect to the components and the resulting composition), can remain without separation or purification as a slurry and be used directly as a polymerization catalyst composition. Thus, the present catalyst composition can be formed by the single-step of mixing the readily available components in an inert liquid and then either directly transferring the formed liquid dispersion to the polymerization reaction zone or placing it in storage under anerobic conditions for latter introduction to the polymerization reaction zone. In this embodiment, the inert liquid used to form the dispersion preferably is chosen from those liquids which (a) are miscible with the liquids used in the polymerization reaction zone, (b) are inert with respect to the solvents, monomer(s) and polymer products contemplated and (c)

are capable of suspending or dispersing Component III (e.g., is a non-solvent for the support-activator agglomerate).

[00183] The present polymerization catalyst composition can be formed in-situ in a liquid phase polymerization reaction zone. The Components I, II and III can be introduced neat or as a solution in an inert liquid, which may be the same liquid as that of the polymerization media. These components may be introduced into the polymerization zone either as solids or as slurries in inert liquids. In all cases, the liquid(s) used to introduce the components forming the present catalyst composition preferably is miscible with the liquid used as the polymerization media.

[00184] In batch polymerization processes, the components forming the present catalyst composition may be introduced prior to, concurrently with or subsequent to the introduction of the olefinic monomer feed. It has been found that the present catalyst composition forms rapidly under normal polymerization conditions to exhibit high catalytic activity and provide a high molecular weight polymer product.

[00185] The amount of Components I and II in the inert liquid hydrocarbon should be controlled to provide a molar ratio of from about 0.01/1 to 10/1 and preferably from 0.1/1 to 2/1 and most preferably from 0.1/1 to 1/1 of Components I and II and a ratio of micromoles of Component I (ligand or the combined precursor reagents) to grams of Component III (support-agglomerate) of typically from about 5:1 to about 500:1, preferably from about 10:1 to about 250:1, and most preferably from about 30:1 to about 100:1 (e.g., 60:1).

[00186] The present composition has unexpectedly been found to exhibit higher polymerization catalytic activity than compositions composed of pre-catalyst that was first formed using the same ligand and transition metal compound and then impregnating the preformed pre-catalyst onto the same support-agglomerate, as used herein. The exact reason for this improvement is not known but is an indication that the present catalyst composition is unique. Further, the present catalyst composition can be effectively used without the need of a cocatalyst, as is believed normally necessary.

[00187] The catalyst composition of the present invention and the scavenger (when used) can be either introduced into the polymerization zone sequentially or simultaneously. When introduced simultaneously, they may be first formed into a common mixture with a hydrocarbon liquid that is miscible with the hydrocarbon liquid in the reaction zone.

[00188] The amount of catalyst composition and the scavenger contained in a hydrocarbon liquid of the polymerization reaction zone may vary but should be controlled to provide an effective amount to sustain the polymerization reaction within the reaction zone, as can be readily determined by those skilled in this art.

[00189] The catalyst composition of the present invention can be used for polymerization, typically addition polymerization, processes wherein one or more monomers are contacted with the present catalyst system (either in its original inert liquid or as separated solid product, as described above) or by direct introduction into the polymerization zone under polymerization conditions.

[00190] Suitable polymerizable monomers include ethylenically unsaturated monomers, acetylenic compounds, conjugated or non-conjugated dienes, and polyenes. Preferred monomers include olefins, for example alpha-olefins having from 2 to 20,000, preferably from 2 to 20, and more preferably from 2 to 8 carbon atoms and combinations of two or more of such alpha-olefins. Particularly suitable alpha-olefins include, for example, ethylene, propylene, 1-butene, 1-pentene, 4-methylpentene-1, 1-hexene, 1-heptene, 1-octene, 1-nonene, 1-decene, 1-undecene, 1-dodecene, 1-tridecene, 1-tetradecene, 1-pentadecene or combinations thereof, as well as long chain vinyl terminated oligomeric or polymeric reaction products formed during the polymerization and C₁₀₋₃₀ α-olefins specifically added to the reaction mixture in order to produce relatively long chain branches in the resulting polymers. Preferably, the alpha-olefins are ethylene, propene, 1-butene, 4-methyl-pentene-1, 1-hexene, 1-octene, and combinations of ethylene and/or propene with one or more of such other alpha-olefins. Other preferred monomers include styrene, halo- or alkyl substituted styrenes, tetrafluoroethylene, vinylcyclobutene, 1,4-hexadiene, dicyclopentadiene, ethylidene norbornene, and 1,7-octadiene. Mixtures of the above-

mentioned monomers may also be employed. The most preferred is ethylene alone or with other alpha-olefins.

[00191] In addition, the polymerization monomers may include functionalized ethylenically unsaturated monomers wherein the functional group is selected from hydroxyl, carboxylic acid, carboxylic acid esters, acetates, ethers, amides, amines and the like.

[00192] More specifically, the catalyst systems described herein are useful to produce polymers using high pressure polymerization, solution polymerization, slurry polymerization, or gas phase polymerization techniques. As used herein, the term polymerization includes copolymerization and terpolymerization, and the terms olefins and olefinic monomers include olefins, alpha-olefins, diolefins, styrenic monomers, acetylenically unsaturated monomers, cyclic olefins, and mixtures thereof.

[00193] For example, polymerization of olefin monomers can be carried out in the gas phase by fluidizing, under polymerization conditions, a bed comprising the target polyolefin powder and particulates of the present catalyst composition using a fluidizing gas stream comprising gaseous monomer. In a solution process the (co)polymerization is typically conducted by introducing the monomer into a solution or suspension of either preformed catalyst composition or the components thereof in a liquid hydrocarbon under conditions of temperature and pressure such that the produced polyolefin forms as a solution in the hydrocarbon diluent. In the slurry process, the temperature, pressure and choice of diluent are such that the produced polymer forms as a suspension in a liquid hydrocarbon diluent.

[00194] The present catalyst system (catalyst composition) can be advantageously employed in a high pressure, solution, slurry or gas phase polymerization process. Methods and apparatus for effecting such polymerization reactions are well known. The catalyst system according to the present invention can be used in similar amounts and under similar conditions generally known for olefin polymerization catalysts. Typically for the slurry process, the temperature is from approximately 0°C to just below the temperature at which the polymer becomes soluble in the polymerization medium. For the gas phase process, the temperature is from approximately 0°C to

just below the melting point of the polymer. For the solution process, the temperature is typically the temperature from which the polymer is soluble in the reaction medium, up to approximately 275°C.

[00195] The pressure used can be selected from a relatively wide range of suitable pressures, e.g., from sub-atmospheric to about 20,000 psi. Preferred pressures can range from atmospheric to about 1000 psi, and most preferred from 50 to 550 psi. In the slurry or particle form process, the process is suitably performed with a liquid inert diluent such as a saturated aliphatic hydrocarbon. The hydrocarbon is typically a C₃ to C₁₀ hydrocarbon, e.g., propane, isobutane or an aromatic hydrocarbon liquid such as benzene, toluene or xylene. The polymer can be recovered directly from the gas phase process, by filtration or evaporation of the slurry from the slurry process, or evaporation of solvent in the solution process.

[00196] The supported catalyst composition of the present invention can be used as the sole catalyst composition in the polymerization of olefins. Alternately, it may be used in combination with at least one supplemental active catalyst species such as metallocene, constrained geometry, bidentate or tridentate ligand containing materials. For example, the catalyst compositions of the present invention may be admixed with at least one supplemental preformed catalyst particulate that utilizes a support-agglomerate formed from a mixture comprising (A) at least one inorganic oxide component, and (B) at least one ion-containing layered component, which optionally has chromium atoms immobilized on and/or within the agglomerate.

[00197] The morphological configuration in which the supplemental catalyst species is employed will typically involve use of at least one supplemental catalytic species absorbed or adsorbed in and/or on (a) a support-agglomerate particles in which chromium is immobilized to within the support-agglomerate; (b) a support-agglomerate particles which do not contain chromium, such as described herein; or (c) mixtures of (a) and (b). Such supplemental catalysts are disclosed in US applications Serial Number 60/287,607; Serial Number 60/287,602; Serial Number 60/287,617; and Serial Number 60/287,600; and concurrently filed and copending U.S. applications having Serial Number _____ (Attorney Docket No. W-9500-02)

Serial Number _____ (Attorney Docket No. W-9509-02); Serial Number _____ (Attorney Docket No. W-9509-02); Serial Number _____ (Attorney Docket No. W-9513-02); Serial Number _____ (Attorney Docket No. W-9568-01); and Serial Number _____ (Attorney Docket No. W-9520-02); the teachings of which are incorporated herein in their entirety by reference.

[00198] For example, the additional particulate may be formed by:

- I. contacting substantially simultaneously or sequentially in a liquid media at least one ligand forming compound comprising at least one bidentate ligand forming compound or at least one tridentate ligand forming compound or mixtures thereof with a transition metal compound and with a support-activator agglomerate comprising (A) at least one inorganic oxide component, and (B) at least one ion-containing layered component. The agglomerate may further have chromium atoms immobilized on and/or within the agglomerate. The resultant particles have the catalyst component(s) contained on such support-activator agglomerate;
- II. contacting substantially simultaneously or sequentially in a liquid media at least one coordination catalyst distinct from that used to form the present composition comprising at least one transition metal bidentate ligand containing compound or at least one transition metal tridentate chelate ligand containing compound or mixtures thereof alone or further with at least one constrained geometry transition metal compound (e.g. a metallocene or its precursors, such as a cyclopentadienyl compound and a metal selected from titanium, zirconium or hafnium) with a support-activator agglomerate comprising (A) at least one inorganic oxide component, and (B) at least one ion-containing layered component. The agglomerate may further have chromium atoms immobilized on and/or within the agglomerate. The resultant particles have the catalyst component(s) contained on such support-activator agglomerates;

- III. contacting substantially simultaneously or sequentially in a liquid media a mixture comprising a) at least one transition metal bidentate ligand containing compound or at least one transition metal tridentate ligand containing compound or mixtures thereof with b) at least one metallocene or constrained geometry transition metal compound (e.g. a metallocene or its precursors, such as a cyclopentadiene or its derivative compounds and a metal selected from titanium, zirconium or hafnium), and with c) a support-activator agglomerate comprising (A) at least one inorganic oxide component, and (B) at least one ion-containing layered component. The agglomerate may further have chromium atoms immobilized on and/or within the agglomerate. The resultant particles have the catalyst component(s) contained on such support-activator agglomerate; or
- IV. contacting substantially simultaneously or sequentially in a liquid media at least one metallocene or constrained geometry transition metal compound (e.g. a metallocene or its precursors, such as a cyclopentadiene or its derivative compounds and a metal selected from titanium, zirconium or hafnium), with a support-activator agglomerate comprising (A) at least one inorganic oxide component, and (B) at least one ion-containing layered component. The agglomerate may further have chromium atoms immobilized on and/or within the agglomerate. The resultant particles have the catalyst component(s) contained on such support-activator agglomerate.

[00199] The present catalyst may be employed with the supplemental catalyst species in any proportion. Thus, one may customize the blend to enhance one or more of the properties of the resultant catalyst composition. For example, if the particular catalyst of the present invention provides a polymer from a particular monomer which exhibits bimodal molecular weight distribution with one modality being substantially greater than the other, a second supported catalyst (supplemental catalyst) may be used to modify the bimodal nature of the resultant polymer product.

The specific identity of the supplemental supported catalyst(s) and the exact ratio to be used to form the admixture will depend on the modification of the property being observed, the nature of each catalyst component and the polymerization conditions contemplated. Such conditions can be determined by simple experimentation by one skilled in this art.

[00200] For example, in an embodiment wherein the present catalyst composition is employed in a mixture with particles of supplemental catalyst specie(s), the present catalyst composition may be a component of a catalyst system that comprises from about 1 to about 99 (e.g. 10 to 90, such as 20 to 85) weight percent of support-agglomerate of the present catalyst composition and from about 95 to about 2 (e.g. 90 to 10, such as 80 to 15, respectively) weight percent of support-activator agglomerate of the second supported supplemental catalyst specie(s) formed from supported bidentate or tridentate transition metal complexes, a metallocene or constrained geometry transition metal compound or precursors of the complex or of the compound., respectively, or mixtures thereof.

[00201] In another embodiment, the present catalyst may be a component of a catalyst composition in which each particle is a composite of the catalyst species of the present invention and at least one supplemental catalyst species. The composite particle may be formed by physically mixing product of the mixture of Components I, II and III as described herein above and a prior formed supplemental catalyst species as also described above and reforming the particulate material or by introducing at least one supplemental catalyst species during the formation of the catalyst species formed according to the present invention. The ratio of present catalyst to supplemental catalyst within each particle may vary widely and will depend on the particular end result desired (catalyst activity, polymer properties, etc.) The composition of the particles may be, for example, from about 5 to about 98 (e.g., 10 to 90, such as 20 to 85) weight percent of a first catalyst component formed from Components I, II and III according to the present invention and from about 95 to about 2 (e.g., 90 to 10, such as 80 to 15, respectively) weight percent of a second supplemental catalyst component. The compounds useful in the formation of each of

the above composite particles are described in the above referenced U. S. patent applications concurrently filed with this application.

[00202] The compounds useful in the formation of each of the above composite particle are described in the above referenced U.S. provisional applications and U.S. patent applications concurrently filed with this application, the teachings of which are incorporated herein by reference.

[00203] It has been unexpectedly found that the present catalyst composition provides polyolefin product (e.g., polyethylene) having bimodal molecular weight distribution. Thus, the present catalyst composition provides an improved polymerization process wherein polymer having bimodal molecular weight distribution can be formed in a single reaction zone.

[00204] All references herein to elements or metals belonging to a certain Group refer to the Periodic Table of the Elements in Hawley's Condensed Chemical Dictionary, 12th Edition. Also, any references to the Group or Groups shall be to the Group or Groups as reflected in this Periodic Table of Elements using the new notation system for numbering groups.

[00205] The following examples are given as specific illustrations of the invention. It should be understood, however, that the invention is not limited to the specific details set forth in the examples. All parts and percentages in the examples, as well as in the remainder of the specification, are by weight unless otherwise specified.

[00206] Further, any range of numbers recited in the specification, such as that representing a particular set of properties, units of measure, conditions, physical states or percentages, is intended to literally incorporate expressly herein by reference or otherwise, any number falling within such range, including any subset of numbers within any range so recited.

Example 1
Preparation of Support-Agglomerate

Part A - Preparation of Base Silica Hydrogel

[00207] Silica gel was prepared by mixing an aqueous solution of sodium silicate and sulfuric acid under suitable agitation and temperature to form a silica sol that sets to a gel in about 8 minutes. The resulting gel was base washed with dilute (about 2 wt.%) ammonia (NH_3) solution at 65.5°C (150°F) for 18 to 36 hours. During this time, the silica gel was cleansed of salt by-products and the surface area was modified. The base wash was followed by a fresh water wash wherein the gel was placed in a re-circulating bath at 82°C.

[00208] The base washed gel was aged at 65-82°C for about 36 hours and a pH of 6 to 7 for one sample designated 1A, and at a pH of 7.5 to 9 for another sample designated 1B. The surface area of the gel was thereby reduced to about $600 \text{ m}^2/\text{g}$ for Sample 1A and to $300 \text{ m}^2/\text{g}$ for Sample 1B. The resulting water washed gel of Samples 1A and 1B have a SiO_2 content of about 35 wt.% with the balance being water, and an Average Particle Size (APS) of Samples 1A and 1B of from 0.5 to 2.0 micron.

Part B(i) - Preparation of Wet Milled Hydrogel Sample 2A (SA $600 \text{ m}^2/\text{g}$)

[00209] A Sample 1A silica gel prepared in accordance with Part A was subjected to wet milling in a sand mill. Sufficient water was then added thereto to make a slurry of 20 wt.% solids. The bulk sample particle size was reduced with a blade mill and further processed through a wet sand mill to reduce the average particle size (APS) to <100 microns. The sample was then sand milled. The slurry was pumped through the sand mill at 1 liter per minute with a media load of 80% (4 liters) zirconia silicate 1.2 mm beads. The average particle size was reduced to 8 and 10 microns and the particle size distribution was 4/8/15 microns for D_{10} , D_{50} and D_{90} . The surface area was $600 \text{ m}^2/\text{g}$. The resulting wet milled sample was designated Sample 2A. Sample 2A had a colloidal content between 20 and 25 wt.% as determined by centrifugation.

Part B(ii) – Preparation of Wet Milled Hydrogel Sample 2B (SA 300 m²/g)

[00210] Example 1, Part B(i) was repeated using base silica gel Sample 1B. The resulting wet milled sample was designated Sample 2B and had a colloidal content between 15 and 30 wt.% as determined by centrifugation and a SA of 300 m²/g. The resulting material was designated Sample 2B.

Part C - Preparation of Dry Milled Sample 3B (SA 300 m²/g)

[00211] A base silica gel Sample 1B prepared in accordance with Part A was subjected to dry milling procedure as follows:

[00212] The sample was spray dried to a moisture content below 10 wt.%. The dried powder sample was then milled to an average particle size (APS) of about 5 microns, a surface area (SA) of still about 300 m²/g, and a N₂ pore volume of 1.5 cc/g. The resulting sample was designated Sample 3B.

Part D - Preparations of Dry Milled Sample 3A (600 m²/g)

[00213] Part C was repeated except that the base silica gel was Sample 1A prepared in accordance with Example 1, Part A. The resulting dry milled sample had a moisture content of less than 10 wt.%, an APS of 5 microns and a SA of 600 m²/g. The resulting sample was designated Sample 3A.

Part E - Preparation of Silica Slurry

[0185] Six different blends (designated Runs 1 to 6) of Sample 2B and Sample 3B were prepared at weight ratios of Sample 3B (dry milled):Sample 2B (wet milled) as reported in Table I. Before blending, Sample 3B was slurried in water to a 20 wt.% solids content using a mixer. The Sample 3B slurry was then added to the 20 wt.% solids content aqueous slurry of Sample 2B at amounts sufficient to achieve the ratios reported in Table I.

TABLE I
Silica Support Slurries
Sample 3B (Dry Milled):Sample 2B (Wet Milled)

Run Number	Ex. No.	Weight % Ratio	Weight Ratio
1	Ex 1 Part E	79/21	3.75:1
2	Ex 1 Part E	78/22	3.50:1
3	Ex 1 Part E	75/25	3.00:1
4	Ex 1 Part E	70/30	2.25:1
5	Ex 1 Part E	60/40	1.50:1
6	Ex 1 Part E	0/100	0:1

Part F - Preparation of Alternate Silica Support Slurries

[00214] Part E was repeated except that Sample 3B ($300\text{ m}^2/\text{g}$) was replaced with Sample 3A ($600\text{ m}^2/\text{g}$) and Sample 2B ($300\text{ m}^2/\text{g}$) was replaced with Sample 2A ($600\text{ m}^2/\text{g}$). The dry milled/wet milled ratios employed are summarized at Table V and the slurries designated Runs 7 to 9.

Table II.

Sample 3A (Dry Milled):Sample 2A (Wet Milled)

Run Number	Weight % Ratio	Weight Ratio
7	75/25	3.00:1
8	60/40	1.50:1
9	0/100	0:1

Part G - Preparation of Clay Slurry

[00215] A montmorillonite clay available from Southern Clay, under the trade names, Montmorillonite BP Colloidal Clay, was obtained. This clay has the following properties as summarized at Table III.

TABLE III
Chemical Composition of Montmorillonite BP Colloidal Clay

Chemical Composition		Physical Properties	
Component	Weight %	Appearance	Tan Powder
SiO ₂	69.5	Apparent Bulk Density	0.45 g/cc
Fe ₂ O ₃	4.4	Surface Area	70 m ² /g
Al ₂ O ₃	19.0	APS	1.5 microns
MgO	2.3	Average Pore Diameter	114 Å
CaO	1.0	Total Pore Volume	0.20 cc/g
Na ₂ O	2.7		
SO ₄	0.6		

Part H - Preparation of Silica/Clay Slurry for Spray Drying

[00216] Each of the silica slurries of Runs 1 to 9 was combined with the clay slurry of Part G in a manner sufficient to control the weight ratio of silica: clay dry solids to be as reported at Table IV. Each slurry was adjusted with acid (sulfuric acid) or base (ammonium hydroxide) to achieve a slurry pH of 7-8.5. The APS of the slurry solids was about 4 to 5 microns, the total dry solids content of the slurry was about 15 to 18 wt.%. The resulting slurries are designated Runs 10 to 18.

TABLE IV

Spray Drying or Tray Drying Slurry and Conditions

Run No.	Ex. No.	Source of Silica (Run Nos.)	Silica:Clay Dry Solids Ratio (w/w)
10	Ex 1 Pt H	1	95:5
11	Ex 1 Pt H	2	90:10
12	Ex 1 Pt H	3	80:20
13	Ex 1 Pt H	4	65:35
14	Ex 1 Pt H	5	50:50
15	Ex 1 Pt H	6	25:75
16	Ex 1 Pt H	7	80:20
17	Ex 1 Pt H	8	50:50
18	Ex 1 Pt H	9	25:75

Part I - Spray Drying of Silica/Clay Slurry

[00217] The pH value of the silica/clay slurry was adjusted and was then pumped to a spray dryer to dry the mixture and to form microspheroidal agglomerates. All spray drying is conducted by using a Bowen 3-ft. diameter spray dryer with inlet-outlet temperatures of 350/150°C and a two-fluid spray nozzle using air at 10-30 psi to atomize the slurry. The air through-put of the Niro is dampened to keep the spray chamber under 7" water vacuum and the slurry is fed at 250-300 cc/min. The product is then collected in the chamber collection pot, located directly under the drying chamber, where the coarsest fraction drops out from air entrainment. Other, smaller fractions go to a cyclone collection pot and the smallest to a baghouse. The chamber material is then screened through 200 to 250 mesh to give the desired APS of 40-55 microns. The Total Volatiles (TV%) at 954.4°C (1750°F) of the spray dried product is in the range of 2-20 wt.%, so further drying in a static bed oven at 150-800°C is then used to lower the total volatiles down to 0.5-5%.

[00218] The total yield of material from the spray dryer chamber collection pot and from screening the same is about 15-20 wt.%.

[00219] Table V below reports silica/clay morphological properties of the resulting agglomerates. The resulting Agglomerate Samples are designated Runs 19 to 27.

TABLE V
Spray Dried Silica/Clay Support-Agglomerate Product Properties

Run No.	Ex. No.	Slurry Source from Table VII (Run No.)	Agglomerate Properties				
			Silica/Clay (Weight Ratio)	APS (microns)	SA (m^2/g)	Pore Vol. (cc/g)	Drying Procedure
19	Ex 1	10	95:5	45	275	1.65	Spray
20	Ex 1	11	90:10	45	268	1.61	Spray
21	Ex 1	12	80:20	45	251	1.48	Spray
22	Ex 1	13	65:35	45	213	1.28	Spray
23	Ex 1	14	50:50	45	185	1.04	Spray
24	Ex 1	15	25:75	45	160	0.64	Spray
25	Ex 1	16	80:20	45	494	1.16	Spray
26	Ex 1	17	50:50	45	322	0.83	Spray
27	Ex 1	18	25:75	45	192	0.54	Spray

Example 2

A. General Procedure for Preparation of Cr Immobilized Support-Agglomerate Material

[00220] The chromium immobilized support-agglomerate was prepared by spray-drying an aqueous mixture (contain about 15% solids) of clay [montmorillonite, APS (average particle size) about 1.5 μm], wet-milled silica powder (APS about 5 μm), sand-milled silica hydrogel (contain ~25% colloid; APS about 5-8 μm), and

chromium acetate solution (1 wt. %). The percentages of the clay, silica powder and hydrogel may be varied to meet the desired specific physical properties of the particles. The SA (surface area) is normally between 185-600 m²/g, while the PV (pore volume-N₂) is from 0.6 - 1.6 cc/g.

B. Spray-Dry Feed Chromium Immobilized Support-Agglomerate (SDF) Catalyst

[00221] A solid slurry of Example I, Table 4, Run 16 was mixed with 1 wt. % chromium acetate solution. This slurry was used as spray dryer feed to give spherical particles having 464 m²/g surface area and 1.24 cc/g pore volume (N₂). The particle size for this material was 53 micron.

Example 3

Oxidation of Chromium Immobilized Support-Agglomerate catalyst

[00222] About 30 c.c. of each sample was fluidized in a quartz tube (4.8 cm O.D.) which had a sintered frit to support the catalyst powder. Dry air previously passed through beds containing activated alumina (typically less than 1 ppm H₂O) was used as fluidizing medium. The dry air flow rate was 40 liter per hour. The fluidized bed was heated at the rate of 400°C/hour to the pre-set temperature of 593°C, which was then kept constant for 5 hours. The quartz tube with the activated catalyst sample was then transferred to a glass container under dry nitrogen for storage. The Cr immobilized support-agglomerate (Example 2 Part B) used for supporting the in-situ formed bi- or tri-dentate ligand containing transition metal complexes were activated in fluidized bed with a stream of dry oxygen.

Example 4**A. Polymerization Method**

[00223] In the slurry polymerization experiments of this and the following examples, unless otherwise indicated, a 2-liter Zipperclave (Autoclave Engineers, Inc.) reactor was rendered inert by heating under vacuum at the polymerization temperature 80°C, for 90 minutes. A reactor charge consisting of a mixture of 400 ml of dry, degassed heptane and the specified amount of tri-isobutylaluminum and the specified supported catalyst system were injected into the reactor. While the reactor contents were stirred at 500 rpm, ethylene was quickly introduced into the reactor until a final reactor pressure of 200 psig was attained. The stated polymerization temperature was maintained by a circulating water bath. Ethylene was supplied on demand via a mass flow controller to maintain the reactor pressure at about 200 psig. After 60 minutes, the ethylene feed was stopped and the reactor cooled to room temperature and vented. The resulting polymer slurry was filtered and washed with methanol and acetone to deactivate any residual catalyst, filtered and dried in a vacuum oven at about 50°C for at least three hours to constant weight. After drying, the polymer was weighed to calculate catalyst activity and a sample of dried polymer was used to determine apparent bulk density according to the procedure of ASTM 1895. Polymer molecular weight and molecular weight distribution data were obtained by GPC, where indicated.

B. Preparation of Cr Immobilized Support-Agglomerate Dual Catalyst (Ni/Cr) Using Organic Diimine Ligand

[00224] A toluene (60ml) slurry of 3-gram dry oxygen-treated Cr immobilized support-agglomerate of Example II, Part B (activation temperature: 540°C) was contacted with 80mg (160 µmole) bi-dentate bis-imine (bis-2,6-diisopropylaniline-1,8-naphthylidene) ligand forming compound and 80 mg (259 µmole) of transition metal compound, NiBr₂(DME) (DME=1,2-dimethoxyethane), at room temperature and agitated overnight (~15 h). The resulting solid slurry was filtered, washed with

heptane (2 x 15ml), and dried under vacuum to give pale orange color free-flowing powder. Yield: 3.15g.

C. Polymerization results using Chromium Immobilized Support-Agglomerate Dual Catalyst.

[00225] 100 mg of Chromium catalyst obtained from Example 4B above was added to a heptane (400 ml) solution that contained specified amount triisobutylaluminum (1M in toluene solution) as listed in TABLE VI below. The catalyst mixture was injected to a pre-heated (50 or 80°C) and pre-vacuumed 2-liter Zipperclave reactor. Ethylene gas was rapidly introduced into the reactor until it reached 200 psig. Ethylene consumption is then gauged by a flow meter to maintain the reactor pressure at 200 psig for one hour. After the reaction, the unreacted ethylene was removed and the heptane/PE slurry was de-activated by the addition of acetone. The supernatant liquid was removed and the granular PE powder was washed with acetone and dried in a hot (60°C) vacuum oven for at least 3 h. Performance of catalyst is listed in Table VI below:

Table VI.
Catalyst Performance of using Cr-Fe dual catalyst.

Run	Polymerization Temp	Al-i-Bu ₃ Used	PE yield	ABD [†]
#	°C	μmol	g	g/cc
1	50	0.6	68	0.30
2	80	0.1	64	0.25

[†]ABD = Apparent polymer bulk density.

[00226] High load melt index was too low to measure for the above two polymers, indicating exceptional high molecule weight polymers were obtained.

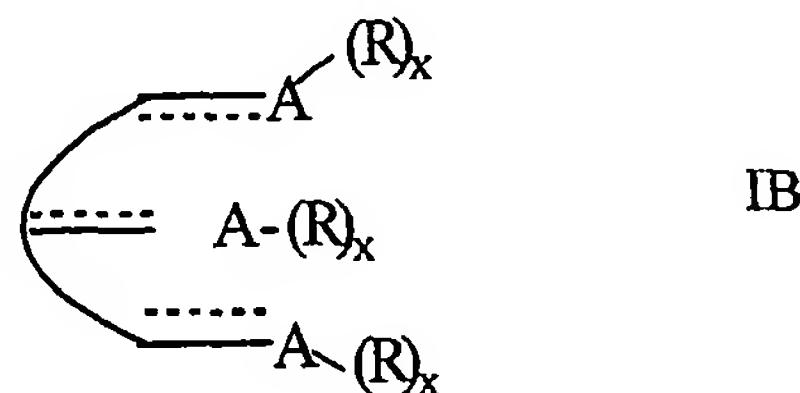
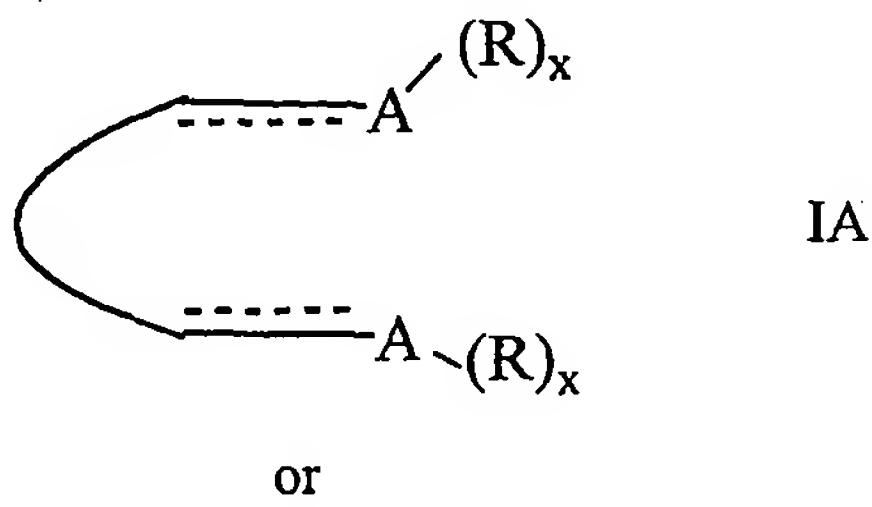
[00227] The principals, preferred embodiments and modes of operation of the present invention have been described in the foregoing application. The invention

which is intended to be protected herein, however, is not to be construed as limited to be particular forms disclosed, since these are to be regarded as illustrative rather than restrictive. Variations and changes may be made by those skilled in the art, without departing from the spirit of the invention.

IN THE CLAIMS:

1. A process for forming a coordination catalyst system useful for the polymerization of olefins comprising:

providing Component I selected from at least one ligand forming compound or precursor compounds capable of forming at least one ligand forming compound wherein said at least one ligand forming compound is represented by at least one of the following formulas IA or IB:



wherein in each of formulas IA and IB above:

each A independently represents an atom of oxygen, sulfur, phosphorous or nitrogen;

each R independently represents hydrogen, an unsubstituted or substituted C₁-C₂₀ hydrocarbyl;

each x independently represents an integer of 0, 1 or 2, provided that when A represents a nitrogen or phosphorous atom x is 1 when said atom A is bonded by a double bond (when --- represents a double bond) and x is 2 when said atom A is bonded by a single bond (when --- represents a single bond) and provided that when

A represents either an oxygen or sulfur atom x is 0 when said atom A is bonded by a double bond; and x is 1 when said atom A is bonded by a single bond; and

the lines joining each A to each other A represent a C₂ to C₉₀ hydrocarbon based group;

providing as Component II at least one a transition metal compound represented by the formula:



wherein

a is an integer of 0, 1 or 2 such that the sum of (a plus 2) equals x,

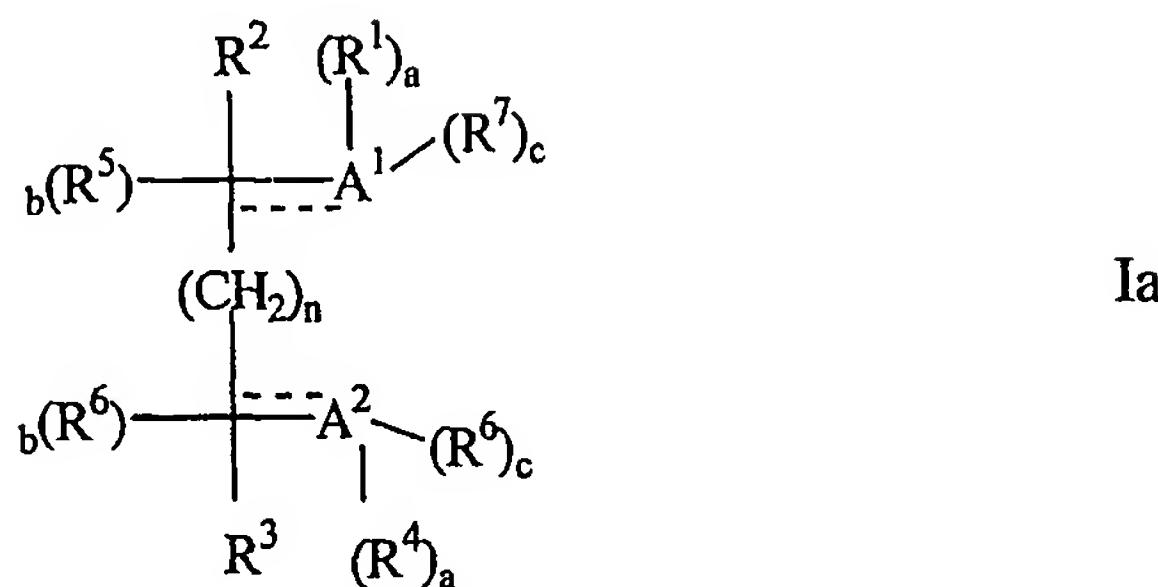
M represents at least one of Group 3 to 10 transition metals of the Periodic Table; and

each L and L', independently represents a member selected from hydrogen, halogen, and hydrocarbon based group associated through a covalent bond to M, or together represent a C₃ to C₂₄ hydrocarbon based group, associated through a covalent or dative bond to M, and which, together with M, constitute a ring or fused ring structure; and

providing as Component III a support-agglomerate composite comprising agglomerates of at least two components comprising (A) at least one inorganic oxide component and (B) at least one ion-containing layered component; and said support-agglomerate further having from 0.1 to 10 weight percent chromium atoms immobilized thereto; or precursor components for said composite selected from (A) at least one inorganic oxide and (B) at least one ion-containing layered component and (C) a chromium compound soluble in an inert liquid in an effective amount to provide 0.1 to 10 weight percent immobilized chromium with respect to the support-agglomerate, said (A) to (B) weight ratio being from 0.25:1 to 99:1;

contacting Components I, II and III in the presence of an inert liquid, said contacting being conducted under conditions to cause Components I, II and III to form an activated catalyst composition.

2. The process of Claim 1 wherein Component I is at least one compound represented by the formula:



wherein

R¹ and R⁴ are each independently selected from an unsubstituted or substituted C₁-C₂₀ hydrocarbyl group, or a fluorinated hydrocarbyl group or together with adjacent groups represent a C₃-C₂₀ hydrocarbylene group;

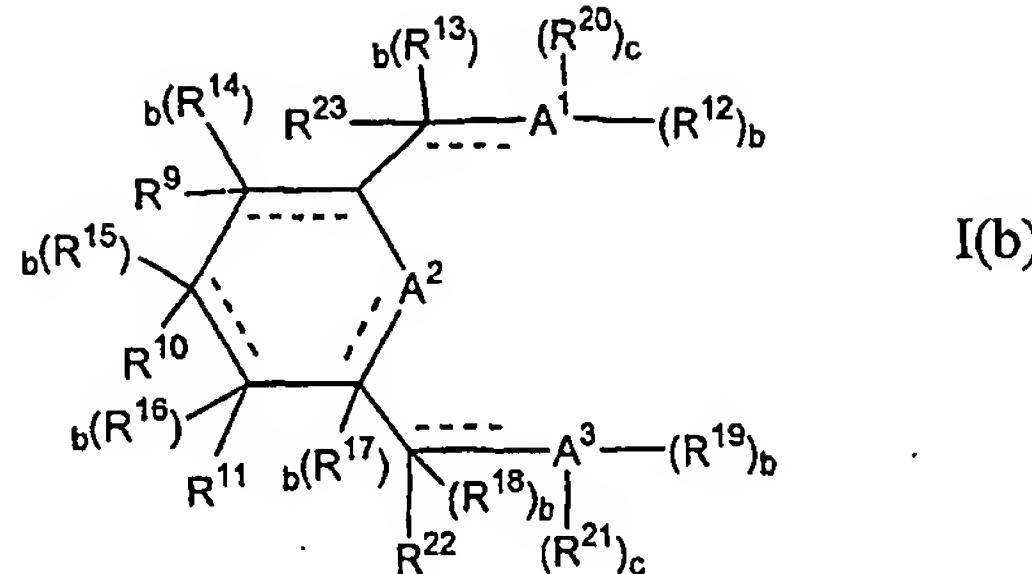
R², R³, R⁵, R⁶, R⁷, and R⁸ are each independently selected from hydrogen, an unsubstituted or substituted C₁-C₂₀ hydrocarbyl group, or any two adjacent R groups together represent an unsubstituted or substituted C₃-C₂₀ hydrocarbylene group;

each A independently represents oxygen, nitrogen, sulfur or phosphorous;

— represents a bond between an A atom and a carbon atom, wherein said bond is selected from a single or a double bond; and

a, b and c each independently represent 0 or 1, provided that when A represents a nitrogen or phosphorous and — represents a double bond then a and b are 0 and c is 1 and where — represents a single bond then a, b and c are each 1, and when A represents oxygen or sulfur and — represents a double bond, then a, b and c are each 0, and when — represents a single bond, then a and b are each 1 and c is 0.

3. The process of Claim 1 wherein Component I is at least one compound represented by the formula:



wherein:

R^{20} and R^{21} are each independently selected from hydrogen, or an unsubstituted or substituted aryl group wherein said substitution is an alkyl or a hetero group which is inert with respect to any contemplated polymerization;

R^{22} and R^{23} are each independently selected from hydrogen, an unsubstituted or substituted C₁-C₂₀ hydrocarbyl;

R^9 to R^{19} are each independently selected from hydrogen, an unsubstituted or substituted C₁-C₂₀ hydrocarbyl or an inert functional group;

each A independently represents oxygen, nitrogen, sulfur or phosphorous;

----- represents a bond between an A atom and a carbon atom, wherein said bond is selected from a single or a double bond; and

b and c are each independently 0 or 1, provided that when A is nitrogen or phosphorous and where ----- represents a double bond, then b is 0 and c is 1 and where ----- represents a single bond, each b and c is 1, and when A represents oxygen or sulfur and where ----- is a double bond then a and b are each 0 and where ----- is a single bond then b is 0 and c is 1.

4. The process of Claim 1 wherein at least one L of the Component II is a halogen atom selected from chlorine or bromine.

5. The process of Claim 2 wherein at least one L of the Component II is a halogen atom selected from chlorine or bromine.

6. The process of Claim 3 wherein at least one L of the Component II is a halogen atom selected from chlorine or bromine.
7. The process of Claim 1 wherein L and L' of the Component II are halogen atoms selected from chlorine or bromine.
8. The process of Claim 1 wherein M of the Component II is a transition metal selected from Fe, Co, Ni, Ru, Rh, Pd, Os, Ir, Pt in the +2 or +3 oxidation state or Ti, V, Cr, Mn, Zr, Hf in the +2, +3 or +4 oxidation state and at least one L is selected from chlorine or bromine.
9. The process of Claim 1 wherein M of the Component II is a transition metal selected from Fe, Co, Ni, or Pd, in the +2 or +3 oxidation state and at least one L is selected from chlorine or bromine.
10. The process of Claim 2 or 3 wherein M of the Component II is a transition metal selected from Fe, Co, Ni, or Pd, in the +2 or +3 oxidation state and at least one L is selected from chlorine or bromine.
11. The process of Claim 2 or 3 wherein the Component II is iron chloride.
12. The process of Claim 1, 2, 3, 4, 5, 6, 7, 8 or 9 wherein Component III is derived from the inorganic oxide (A) selected from SiO_2 , Al_2O_3 , AlPO_4 , MgO , TiO_2 , ZrO_2 , $\text{SiO}_2 \cdot \text{Al}_2\text{O}_3$, $\text{MgO} \cdot \text{SiO}_2 \cdot \text{Al}_2\text{O}_3$, $\text{SiO}_2 \cdot \text{TiO}_2 \cdot \text{Al}_2\text{O}_3$, $\text{SiO}_2 \cdot \text{Cr}_2\text{O}_3 \cdot \text{Al}_2\text{O}_3$ or $\text{SiO}_2 \cdot \text{Cr}_2\text{O}_3 \cdot \text{TiO}_2$ and mixtures thereof.
13. The process of Claim 10 wherein Component III is derived from the inorganic oxide (A) selected from SiO_2 , Al_2O_3 , AlPO_4 , MgO , TiO_2 , ZrO_2 , $\text{SiO}_2 \cdot \text{Al}_2\text{O}_3$, $\text{MgO} \cdot \text{SiO}_2 \cdot \text{Al}_2\text{O}_3$, $\text{SiO}_2 \cdot \text{TiO}_2 \cdot \text{Al}_2\text{O}_3$, $\text{SiO}_2 \cdot \text{Cr}_2\text{O}_3 \cdot \text{Al}_2\text{O}_3$ or $\text{SiO}_2 \cdot \text{Cr}_2\text{O}_3 \cdot \text{TiO}_2$ and mixtures thereof.

14. The process of Claim 12 wherein the ion-containing layered component (B) of Component III is derived from at least one ion containing layered material having interspaces between the layers and capable of exhibiting Lewis acidity, said layered material having a cationic component and an anionic component, wherein said cationic component is present within the interspace of the layered material and said layered material is intimately dispersed with said inorganic oxide component of the Component III:

15. The process of Claim 13 wherein the ion-containing layered component (B) of Component III is derived from at least one ion containing layered material having interspaces between the layers and capable of exhibiting Lewis acidity, said layered material having a cationic component and an anionic component, wherein said cationic component is present within the interspace of the layered material and said layered material is intimately dispersed with said inorganic oxide component of the Component III.

16. The process of Claim 12 wherein at least about 80 weight percent of the inorganic oxide (A) of the Component III comprises silica gel.

17. The process of Claim 1 wherein in each of the formula IA and IB:
each A in IA and at least two A's in IB represent nitrogen;
each R independently represents a C₃-C₂₀ hydrocarbyl group;
each x independently represents 1 or 2; and
the lines joining each A to each other A represents a C₃-C₂₀ hydrocarbylene radical.

18. The process of Claim 2 wherein: R¹ and R⁴ are each independently selected from an unsubstituted or substituted C₃-C₂₀ hydrocarbyl group; and each A independently represents oxygen or nitrogen

19. The process of Claim 3 wherein each A represents oxygen or nitrogen; R²⁰ and R²¹ are each independently selected from an unsubstituted or substituted aryl group; R¹² to R¹⁹ is each independently selected from an unsubstituted or substituted hydrocarbyl; R⁹, R¹⁰ and R¹¹ are hydrogen; R²² and R²³ are independently selected from hydrogen or methyl.
20. The process of Claim 2 wherein the Component III, (B) is derived from layered clay and clay minerals having a three dimensional structure wherein stronger bonds are present in two of the three dimensions and have a negative charge of less than 0.
21. The process of Claim 3 wherein the Component III, (B) is derived from layered clay and clay minerals having a three dimensional structure wherein stronger bonds are present in two of the three dimensions and have a negative charge of less than 0.
22. The process of Claim 14 wherein the chromium atoms are covalently bonded to oxygen atoms of the support-agglomerate.
23. The process of Claim 15 wherein the chromium atoms are covalently bonded to oxygen atoms of the support-agglomerate.
24. The process of Claim 2 wherein the Component III comprises component (A) to (B) in a weight ratio of from 0.025:1 to 99:1 and has a surface area of from about 20 to about 800 m²/g; a bulk density of at least about 0.15g/ml; an average pore diameter of from 30 to 300 Å; a total pore volume of from about 0.1 to about 2 cc/g; and an average particle size of from about 4 to about 250 microns.
25. The process of Claim 3 wherein the Component III comprises component (A) to (B) in a weight ratio of from 0.025:1 to 99:1 and has a surface area of from about

20 to about 800 m²/g; a bulk density of at least about 0.15g/ml; an average pore diameter of from 30 to 300 Å; a total pore volume of from about 0.1 to about 2 cc/g; and an average particle size of from about 4 to about 250 microns.

26. The process of Claim 1, 2, 3, 4, 5, 6, 7, 8 or 9 wherein Components (I), (II) and (III) are contacted substantially simultaneously in a liquid medium.

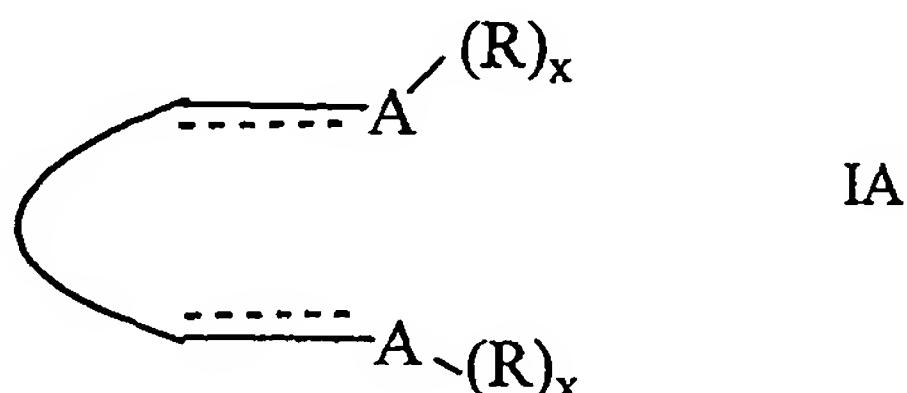
27. The process of Claim 1, 2, 3, 4, 5, 6, 7, 8 or 9 wherein Components (II) and (III) are contacted substantially simultaneously in a liquid medium follows by contact with Component (I).

28. The process of Claim 1, 2, 3, 4, 5, 6, 7, 8 or 9 wherein Components (I) and (III) are contacted substantially simultaneously in a liquid medium followed by contact with Component (II)

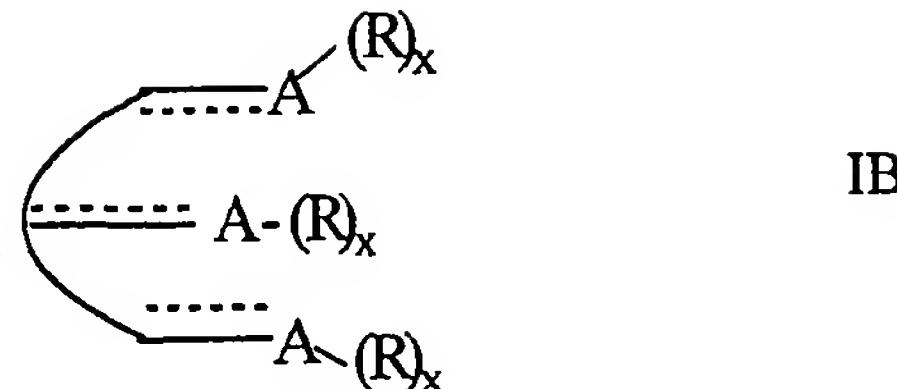
29. The process of Claim 1, 2, 3, 4, 5, 6, 7, 8 or 9 wherein Component (I) comprises precursor reagents capable of forming said bidentate or tridentate ligand compound.

30. A catalyst useful for the polymerization of olefins formed by contacting substantially simultaneously in an inert liquid:

Component (I) selected from at least one ligand forming compound or precursor compounds capable of forming at least one ligand forming compound, wherein said at least one ligand forming compound is represented by the general formula:



or



wherein in each of formulas IA and IB above:

each A independently represents an atom of oxygen, sulfur, phosphorous or nitrogen;

each R independently represents hydrogen, an unsubstituted or substituted C₁-C₂₀ hydrocarbyl;

each x independently represents an integer of 0, 1 or 2, provided that when A represents a nitrogen or phosphorous atom x is 1 when said atom A is bonded by a double bond (when ___ represents a double bond) and x is 2 when said atom A is bonded by a single bond (when ___ represents a single bond) and provided that when A represents either an oxygen or sulfur atom x is 0 when said atom A is bonded by a double bond; and x is 1 when said atom A is bonded by a single bond; and

the lines joining each A to each other A represent a C₂ to C₉₀ hydrocarbon based group; with

Component(II) comprising a transition metal compound represented by the formula:



wherein

a is an integer of 0, 1 or 2 such that a plus 2 equals x,

M represents at least one of Group 3 to 10 transition metals of the Periodic Table; and

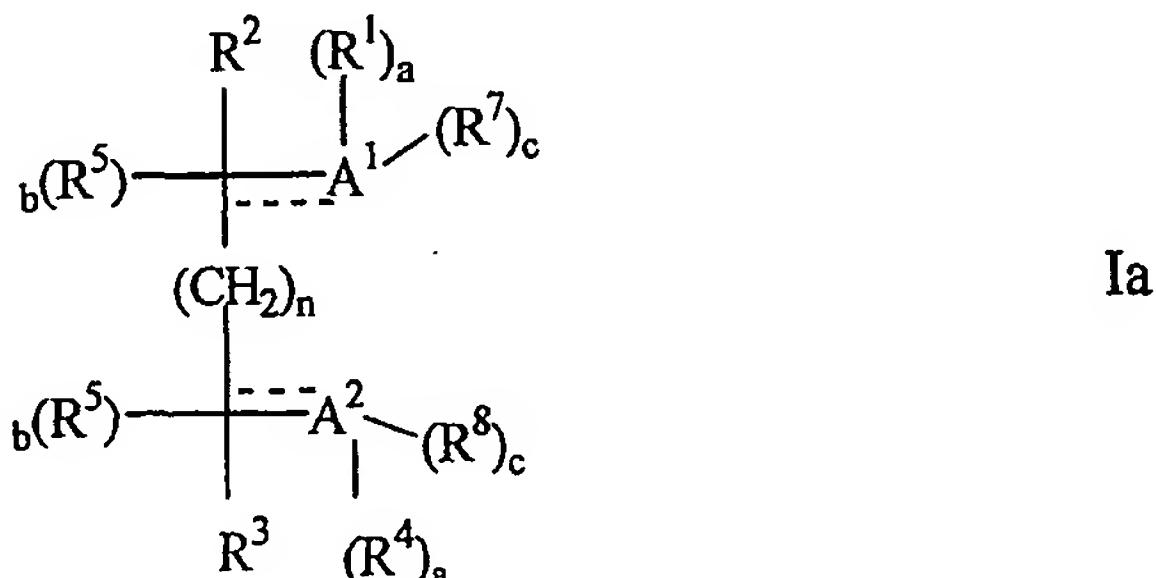
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each L and L', independently represents a group selected from hydrogen, halogen, and hydrocarbon based group associated through a covalent bond to M, or together represent a C₃ to C₂₄ hydrocarbon based group, associated through a covalent or dative bond to M, and which, together with M, constitute a ring or fused ring structure; and with

(III) a support-agglomerate composite comprising agglomerates of at least two components comprising (A) at least one inorganic oxide component and (B) at least one ion-containing layered component and said support-agglomerate further having chromium atoms immobilized thereto; or precursor components for said composite selected from (A) at least one inorganic oxide and (B) at least one ion-containing layered component and (c) a chromium compound soluble in an inert liquid in an effective amount to provide 0.1 to 10 weight percent immobilized chromium with respect to the support-agglomerate.

said contacting being conducted under conditions sufficient to have Component I, II and II form an activated catalyst composition.

31. The catalyst of Claim 30 wherein the Component I is at least one compound represented by the formula:



a, b and c each independently represent 0 or 1;

R^1 and R^4 are each independently selected from an unsubstituted or substituted C_1 - C_{20} hydrocarbyl group, or a fluorinated hydrocarbyl group or together with adjacent groups represent a C_3 - C_{20} hydrocarbylene group;

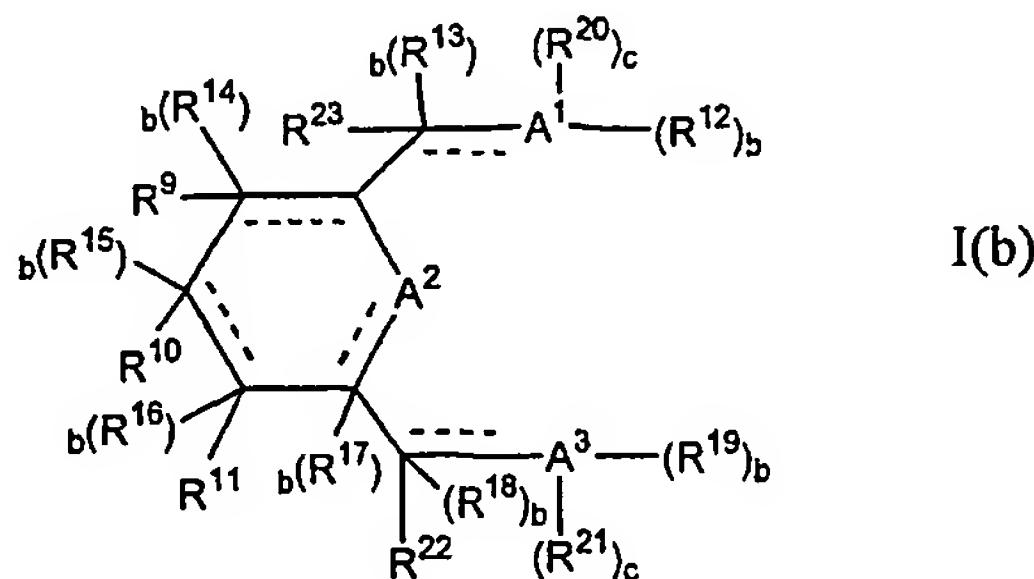
R^2 , R^3 , R^5 , R^6 , R^7 , and R^8 are each independently selected from hydrogen, an unsubstituted or substituted C_1 - C_{20} hydrocarbyl group, or any two adjacent R groups together represent an unsubstituted or substituted C_3 - C_{20} hydrocarbylene group;

each A independently represents oxygen, nitrogen, sulfur or phosphorous; and

— represents a bond between an A atom and a carbon atom, wherein said bond is selected from a single or a double bond; and

a, b and c each independently represent 0 or 1, provided that when A represents a nitrogen or phosphorous and — represents a double bond then a and b are 0 and c is 1 and where — represents a single bond then a, b and c are each 1, and when A represents oxygen or sulfur and — represents a double bond, then a, b and c are each 0, and when — represents a single bond, then a and b are each 1 and c is 0.

32. The catalyst of Claim 30 wherein the Component I is at least one compound represented by the formula:



wherein:

R^{20} and R^{21} are each independently selected from hydrogen, or an unsubstituted or substituted aryl group wherein said substitution is an alkyl or a hetero group which is inert with respect to any contemplated polymerization;

R^{22} and R^{23} are each independently selected from hydrogen, an unsubstituted or substituted C_1 - C_{20} hydrocarbyl;

R^9 to R^{19} are each independently selected from hydrogen, an unsubstituted or substituted C₁-C₂₀ hydrocarbyl or an inert functional group;

each A independently represents oxygen, nitrogen, sulfur or phosphorous;

----- represents a bond between atoms wherein said bond is selected from a single or a double bond; and

b and c are each independently 0 or 1; provided that when A is nitrogen or phosphorous and where ----- represents a double bond, then b is 0 and c is 1 and where ----- represents a single bond each b and c is 1, and when A represents oxygen or sulfur and where ----- is a double bond then a and b are each 0 and where ----- is a single bond then b is 0 and c is 1.

33. The catalyst of Claim 30 wherein at least one L of the Component II is a halogen atom selected from chlorine or bromine.

34. The catalyst of Claim 31 wherein at least one L of the Component II is a halogen atom selected from chlorine or bromine.

35. The catalyst of Claim 32 wherein at least one L of the Component II is a halogen atom selected from chlorine or bromine.

36. The catalyst of Claim 30 wherein L and L' of the Component II are halogen atoms selected from chlorine or bromine.

37. The catalyst of Claim 30 wherein M of the Component II is a transition metal selected from Fe, Co, Ni, Ru, Rh, Pd, Os, Ir, Pt in the +2 or +3 oxidation state or Ti, V, Cr, Mn, Zr, Hf in the +2, +3 or +4 oxidation state and at least one L is selected from chlorine or bromine.

38. The catalyst of Claim 30 wherein M of the Component II is a transition metal selected from Fe, Co, Ni, or Pd, in the +2 or +3 oxidation state and at least one L is selected from chlorine or bromine.

39. The catalyst of Claim 31 or 32 wherein M of the Component II is a transition metal selected from Fe, Co, Ni, or Pd, in the +2 or +3 oxidation state and at least one L is selected from chlorine or bromine.

40. The catalyst of Claim 31 or 32 wherein the Component II is iron chloride.

41. The catalyst of Claim 30, 31, 32, 33, 34, 35 36, 37 or 38 wherein Component III is derived from the inorganic oxide (A) selected from SiO_2 , Al_2O_3 , AlPO_4 , MgO , TiO_2 , ZrO_2 , $\text{SiO}_2 \cdot \text{Al}_2\text{O}_3$, $\text{MgO} \cdot \text{SiO}_2 \cdot \text{Al}_2\text{O}_3$, $\text{SiO}_2 \cdot \text{TiO}_2 \cdot \text{Al}_2\text{O}_3$, $\text{SiO}_2 \cdot \text{Cr}_2\text{O}_3 \cdot \text{Al}_2\text{O}_3$ or $\text{SiO}_2 \cdot \text{Cr}_2\text{O}_3 \cdot \text{TiO}_2$ and mixtures thereof.

42. The catalyst of Claim 39 wherein Component III is derived from the inorganic oxide (A) selected from SiO_2 , Al_2O_3 , AlPO_4 , MgO , TiO_2 , ZrO_2 , $\text{SiO}_2 \cdot \text{Al}_2\text{O}_3$, $\text{MgO} \cdot \text{SiO}_2 \cdot \text{Al}_2\text{O}_3$, $\text{SiO}_2 \cdot \text{TiO}_2 \cdot \text{Al}_2\text{O}_3$, $\text{SiO}_2 \cdot \text{Cr}_2\text{O}_3 \cdot \text{Al}_2\text{O}_3$ or $\text{SiO}_2 \cdot \text{Cr}_2\text{O}_3 \cdot \text{TiO}_2$ and mixtures thereof.

43. The process of Claim 41 wherein the ion-containing layered component (B) of Component III is derived from at least one ion containing layered material having interspaces between the layers of capable of exhibiting Lewis acidity, said layered material having a cationic component and an anionic component, wherein said cationic component is present within the interspace of the layered material and said layered material is intimately dispersed with said inorganic oxide component of the Component III.

44. The process of Claim 42 wherein the ion-containing layered component (B) of Component III is derived from at least one ion containing layered material having

interspaces between the layers of capable of exhibiting Lewis acidity, said layered material having a cationic component and an anionic component, wherein said cationic component is present within the interspace of the layered material and said layered material is intimately dispersed with said inorganic oxide component of the Component III.

45. The catalyst of Claim 41 wherein the ion-containing layered component (B) of Component III is derived from at least one ion containing layered material having interspaces between the layers and capable of exhibiting Lewis acidity, said layered material having a cationic component and an anionic component, wherein said cationic component is present within the interspace of the layered material and said layered material is intimately dispersed with said inorganic oxide component of the Component III.

46. The catalyst of Claim 30 wherein at least about 80 weight percent of the inorganic oxide component (A) of the support activator is composed of a silica gel.

47. The catalyst of Claim 30 wherein in each of the formula IA and IB:
each A in IA and at least two A's in IB represent nitrogen;
each R independently represents a C₃-C₂₀ hydrocarbyl group;
each x independently represents 1 or 2; and
the lines joining each A to each other A represents a C₃-C₂₀ hydrocarbylene radical.

48. The catalyst of Claim 31 wherein R¹ and R⁴ are each independently selected from an unsubstituted or substituted C₃-C₂₀ hydrocarbyl group; and each A independently represents oxygen or nitrogen

49. The process of Claim 32 wherein each A is selected from oxygen or nitrogen; R²⁰ and R²¹ are each independently selected from an unsubstituted or substituted aryl group; R¹² to R¹⁹ is each independently selected from an unsubstituted or substituted

hydrocarbyl; R⁹, R¹⁰ and R¹¹ are hydrogen; R²² and R²³ are independently selected from hydrogen or methyl.

50. The catalyst of Claim 30 wherein the Component III, (B) is derived from layered clay and clay minerals having a three dimensional structure wherein stronger bonds are present in two of the three dimensions and have a negative charge of less than 0.

51. The catalyst of Claim 31 or 32 wherein the Component III, (B) is derived from layered clay and clay minerals having a three dimensional structure wherein stronger bonds are present in two of the three dimensions and have a negative charge of less than 0.

52. The catalyst of Claim 30 wherein the Component III comprises component (A) to (B) in a weight ratio of from 0.025:1 to 99:1 and has a surface area of from about 20 to about 800 m²/g; a bulk density of at least about 0.15g/ml; an average pore diameter of from 30 to 300 Å; a total pore volume of from about 0.1 to about 2 cc/g; and an average particle size of from about 4 to about 250 microns.

53. The catalyst of Claim 31 wherein the Component III comprises component (A) to (B) in a weight ratio of from 0.025:1 to 99:1 and has a surface area of from about 20 to about 800 m²/g; a bulk density of at least about 0.15g/ml; an average pore diameter of from 30 to 300 Å; a total pore volume of from about 0.1 to about 2 cc/g; and an average particle size of from about 4 to about 250 microns.

54. The catalyst of Claim 30, 31, 32, 33, 34, 35 36, 37 or 38 wherein Components(I), (II) and (III) are contacted substantially simultaneously in a liquid medium.

55. The catalyst of Claim 30, 31, 32, 33, 34, 35 36, 37 or 38 wherein Components (II) and (III) are contacted substantially simultaneously in a liquid medium follows by contact with Component (I).
56. The catalyst of Claim 30, 31, 32, 33, 34, 35 36, 37 or 38 wherein Components (I) and (III) are contacted substantially simultaneously in a liquid medium followed by contact with Component (II).
57. The catalyst of Claim 30, 31, 32, 33, 34, 35 36, 37 or 38 wherein Component (I) comprises precursor reagents capable of forming said bidentate or tridentate ligand.
58. A process for the polymerization of olefins comprising contacting in a polymerization zone at least one olefinic compound with the catalyst composition of Claim 30, 31, 32, 33, 34, 35 36, 37 or 38.
59. A process for the polymerization of olefins comprising contacting in a polymerization zone at least one olefinic compound with the catalyst composition of Claim 39.
60. A process for the polymerization of olefins comprising contacting in a polymerization zone at least one olefinic compound with the catalyst composition of Claim 41.
61. A process for the polymerization of olefins comprising contacting in a polymerization zone at least one olefinic compound with the catalyst composition of Claim 43.

62. A process for the polymerization of olefins comprising contacting in a polymerization zone at least one olefinic compound with the catalyst composition of Claim 54.

63. A process for the polymerization of olefins comprising contacting in a polymerization zone at least one olefinic compound with the catalyst composition of Claim 55.

64. A process for the polymerization of olefins comprising contacting in a polymerization zone at least one olefinic compound with the catalyst composition of Claim 56.

65. A process for the polymerization of olefins comprising contacting in a polymerization zone at least one olefinic compound with the catalyst composition of Claim 57.

66. The process of Claim 58 wherein the polymerization zone further contains a compound represented by the formula:



wherein D represents an element of the Group 1, 2 or 13 of the Periodic Table, or a tin atom or a zinc atom; each R²⁰ independently represents a hydrogen atom, a halogen atom, a C₁ to C₂₄ hydrocarbyl or halogenated hydrocarbyl group, and s is the oxidation number of D.

67. The process of Claim 59 wherein the polymerization zone further contains a compound represented by the formula:



wherein D represents an element of the Group 1, 2 or 13 of the Periodic Table, or a tin atom or a zinc atom; each R²⁰ independently represents a hydrogen atom, a halogen atom, a C₁ to C₂₄ hydrocarbyl or halogenated hydrocarbyl group, and s is the oxidation number of D.

68. The process of Claim 58 wherein the polymerization zone further contains at least one supplemental particulate catalyst comprising:

- i) a pre-catalyst component selected from a supported bidentate transition metal complex or tridentate transition metal complex, a metallocene transition metal complex or constrained geometry transition metal complex or precursors of said complexes, or mixtures thereof; and
- ii) a support for said pre-catalyst composed of a support-activator agglomerate comprising (A) at least one inorganic oxide component selected from SiO₂•Al₂O₃, MgO•SiO₂•Al₂O₃, SiO₂•TiO₂•Al₂O₃, SiO₂•Cr₂O₃•Al₂O₃ or SiO₂•Cr₂O₃•TiO₂ and mixtures thereof, and (B) at least one ion-containing layered component having interspaces between the layers and capable of exhibiting Lewis acidity, said layered material having a cationic component and an anionic component, wherein said cationic component is present within the interspace of the layered material and said layered material is intimately dispersed with said inorganic oxide component of the Component III..

69. The process of Claim 59 wherein the polymerization zone further contains at least one supplemental particulate catalyst comprising:

- i) at least one pre-catalyst component selected from a supported bidentate transition metal complex, a tridentate transition metal complex, a metallocene transition metal complex or a constrained geometry

transition metal complex or precursors of said complexes, or mixtures thereof; and

- ii) a support for said pre-catalyst composed of a support-activator agglomerate comprising (A) at least one inorganic oxide component selected from $\text{SiO}_2\text{-Al}_2\text{O}_3$, $\text{MgO}\text{-SiO}_2\text{-Al}_2\text{O}_3$, $\text{SiO}_2\text{-TiO}_2\text{-Al}_2\text{O}_3$, $\text{SiO}_2\text{-Cr}_2\text{O}_3\text{-Al}_2\text{O}_3$ or $\text{SiO}_2\text{-Cr}_2\text{O}_3\text{-TiO}_2$ and mixtures thereof, and (B) at least one ion-containing layered component having interspaces between the layers and capable of exhibiting Lewis acidity, said layered material having a cationic component and an anionic component, wherein said cationic component is present within the interspace of the layered material and said layered material is intimately dispersed with said inorganic oxide component of the Component III.

70. The process of Claim 68 wherein the support-activator agglomerate of said at least one supplemental particulate catalyst has chromium atoms immobilized to the support-activator agglomerate.

71. The process of Claim 69 wherein the support-activator agglomerate of said at least one supplemental particulate catalyst has chromium atoms immobilized to the support-activator agglomerate.

INTERNATIONAL SEARCH REPORT

International Application No

PCT/US 02/11370

A. CLASSIFICATION OF SUBJECT MATTER
 IPC 7 C08F10/02 C08F4/02 C08F4/70

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHEDMinimum documentation searched (classification system followed by classification symbols)
 IPC 7 C08F B01J C07F

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the International search (name of data base and, where practical, search terms used)

EPO-Internal, WPI Data

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y	EP 0 874 006 A (MITSUBISHI CHEM CORP) 28 October 1998 (1998-10-28) the whole document ---	1-71
Y	WO 01 25149 A (CARNAHAN EDMUND M ; JOVANOVIC ZORAN R (US); GARCES JUAN M (US); SUN) 12 April 2001 (2001-04-12) the whole document ---	1-71
P,A	WO 01 32722 A (GRACE W R & CO) 10 May 2001 (2001-05-10) the whole document ---	1-71
P,A	WO 01 42320 A (DOW CHEMICAL CO) 14 June 2001 (2001-06-14) the whole document ---	1-71
		-/-

 Further documents are listed in the continuation of box C. Patent family members are listed in annex.

* Special categories of cited documents :

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- *T* later document published after the International filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

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- *&* document member of the same patent family

Date of the actual completion of the International search

Date of mailing of the international search report

11 July 2002

19/07/2002

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Authorized officer

Balmer, J-P

INTERNATIONAL SEARCH REPORT

International Application No

PCT/US 02/11370

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
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